CHBE320 LECTURE V LAPLACE TRANSFORM AND TRANSFER FUNCTION

Professor Dae Ryook Yang

Fall 2021 Dept. of Chemical and Biological Engineering **Korea University**

CHBE320 Process Dynamics and Control

Korea University 5-1

SOLUTION OF LINEAR ODE

- 1st-order linear ODE
 - **Integrating factor:** For $\frac{dx}{dt} + a(t)x = f(t)$, i.f. = exp($\int a(t)dt$) $[xe^{\int a(t)dt}]' = f(t)e^{\int a(t)dt} \quad \longrightarrow \quad x(t) = [\int f(t)e^{\int a(t)dt} \, dt + C]e^{-\int a(t)dt}$
- · High-order linear ODE with constant coeffs.
 - Modes: roots of characteristic equation

For
$$a_2x'' + a_1x' + a_0x = f(t)$$
,
 $a_2p^2 + a_1p + a_0 = a_2(p - p_1)(p - p_2) = 0$

- Depending on the roots, modes are
 - Distinct roots: (e^{-p_1t}, e^{-p_2t}) • **Double roots:** (e^{-p_1t}, te^{-p_1t})

Solution is a linear combination of modes and the coefficients are decided by the initial conditions.

• Imaginary roots: $(e^{-\alpha t}\cos\beta t, e^{-\alpha t}\sin\beta t)$

Many other techniques for different cases

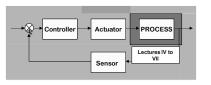
CHBE320 Process Dynamics and Control

Korea University 5-3

Road Map of the Lecture V

Laplace Transform and Transfer functions

- Definition of Laplace transform
- Properties of Laplace transform
- Inverse Laplace transform
- Definition of transfer function
- How to get the transfer functions
- Properties of transfer function



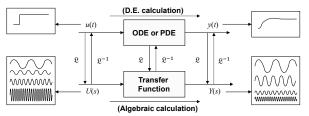
CHBE320 Process Dynamics and Control

Korea University 5-2

LAPLACE TRANSFORM FOR LINEAR ODE **AND PDE**

Laplace Transform

- Not in time domain, rather in frequency domain
- Derivatives and integral become some operators.
- ODE is converted into algebraic equation
- PDE is converted into ODE in spatial coordinate
- Need inverse transform to recover time-domain solution



CHBE320 Process Dynamics and Control

DEFINITION OF LAPLACE TRANSFORM

Definition

$$F(s) = \mathfrak{L}{f(t)} \triangleq \int_0^\infty f(t)e^{-st}dt$$

- F(s) is called *Laplace transform* of f(t).
- f(t) must be piecewise continuous.
- F(s) contains no information on f(t) for t < 0.
- The past information on f(t) (for t < 0) is irrelevant.
- The s is a complex variable called "Laplace transform variable"

Inverse Laplace transform

$$f(t) = \mathfrak{L}^{-1}\{F(s)\}\$$

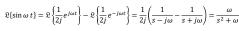
- \mathfrak{L} and \mathfrak{L}^{-1} are linear. $\mathfrak{L}\{af_1(t) + bf_2(t)\} = aF_1(s) + bF_2(s)$

CHBE320 Process Dynamics and Control

Korea University 5-5

Trigonometric functions

- **Euler's Identity:** $e^{j\omega t} \triangleq \cos \omega t + j \sin \omega t$ $\cos \omega t = \frac{1}{2} \left(e^{j\omega t} + e^{-j\omega t} \right) \qquad \sin \omega t = \frac{1}{2j} \left(e^{j\omega t} - e^{-j\omega} \right)$



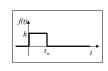
$$\mathfrak{L}\{\cos\omega\,t\} = \mathfrak{L}\left\{\frac{1}{2}e^{j\omega t}\right\} + \mathfrak{L}\left\{\frac{1}{2}e^{-j\omega}\right\} = \frac{1}{2}\left(\frac{1}{s-j\omega} + \frac{1}{s+j\omega}\right) = \frac{s}{s^2 + \omega^2}$$

• Rectangular pulse, P(t)

Rectangular pulse,
$$P(t)$$

$$f(t) = P(t) = \begin{cases} 0 & \text{for } t > t_w \\ h & \text{for } t_w \ge t \ge 0 \\ 0 & \text{for } t < 0 \end{cases}$$

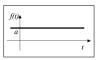
$$\mathfrak{Q}\{P(t)\} = \int_0^{t_w} h e^{-st} dt = -\frac{h}{s} e^{-st} \Big|_0^{t_w} = \frac{h}{s} (1 - e^{-t_w s})$$



LAPLACE TRANSFORM OF FUNCTIONS

Constant function. a

$$\mathfrak{L}\{a\} = \int_{0}^{\infty} ae^{-s} dt = -\frac{a}{s}e^{-st}\Big|_{0}^{\infty} = 0 - \left(-\frac{a}{s}\right) = \frac{a}{s}$$



• Step function, S(t)

$$f(t) = S(t) = \begin{cases} 1 & \text{for } t \ge 0 \\ 0 & \text{for } t < 0 \end{cases}$$

$$\mathfrak{L}\{S(t)\} = \int_0^\infty e^{-s} dt = -\frac{1}{s} e^{-st} \bigg|_0^\infty = 0 - \left(-\frac{1}{s}\right) = \frac{1}{s}$$



• Exponential function, e-bt

$$\mathfrak{L}\{e^{-bt}\} = \int_0^\infty e^{-b} e^{-s} dt = \frac{-1}{s+b} e^{-(b+s)t} \Big|_0^\infty = \frac{1}{s+b}$$



CHBE320 Process Dynamics and Control

Korea University 5-6

• Impulse function, $\delta(t)$

$$f(t) = \delta(t) = \lim_{t_w \to 0} \begin{cases} 0 & \text{for } t > t_w \\ 1/t_w & \text{for } t_w \ge t \ge 0 \\ 0 & \text{for } t < 0 \end{cases}$$

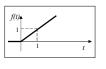


$$\mathfrak{L}\{\delta(t)\} = \lim_{t_w \to 0} \int_0^{t_w} \frac{1}{t_w} e^{-st} dt = \lim_{t_w \to 0} \frac{1}{t_w s} (1 - e^{-t_w s}) = 1$$

$$\left(\text{L'Hospital's rule: } \lim_{t \to 0} \frac{f(t)}{g(t)} = \lim_{t \to 0} \frac{f'(t)}{g'(t)} \right)$$

Ramp function, t

$$\begin{aligned} & \mathcal{Q}\{t\} = \int_0^\infty t e^{-s} \, dt \\ & = \frac{t}{-s} e^{-st} \Big|_0^\infty - \int_0^\infty \frac{e^{-s}}{-s} \, dt = \frac{1}{s} \int_0^\infty e^{-st} \, dt = \frac{1}{s^2} \end{aligned}$$

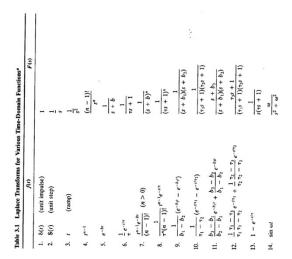


- (Integration by part: $\int_{0}^{\infty} f' \cdot g dt = f \cdot g \Big|_{0}^{\infty} \int_{0}^{\infty} f \cdot g' dt$)
- Refer the Table 3.1 (Seborg et al.) for other functions

CHBE320 Process Dynamics and Control

Korea University 5-7

CHBE320 Process Dynamics and Control



CHBE320 Process Dynamics and Control

Korea University 5-9

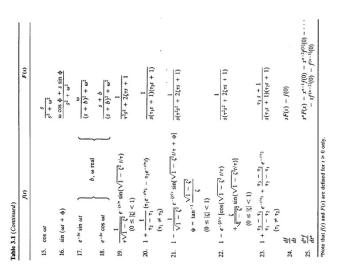
PROPERTIES OF LAPLACE TRANSFORM

Differentiation

$$\begin{split} & \mathfrak{L}\left\{\frac{df}{dt}\right\} = \int_{0}^{\infty} f' \cdot e^{-st} dt = f(t)e^{-st}\Big|_{0}^{\infty} - \int_{0}^{\infty} f \cdot (-s)e^{-st} dt \qquad \text{(by i. b. p.)} \\ & = s \int_{0}^{\infty} f \cdot e^{-st} dt - f(0) = sF(s) - f(0) \\ & \mathfrak{L}\left\{\frac{d^{2}f}{dt^{2}}\right\} = \int_{0}^{\infty} f'' \cdot e^{-st} dt = f(t)'e^{-st}\Big|_{0}^{\infty} - \int_{0}^{\infty} f' \cdot (-s)e^{-st} dt = s \int_{0}^{\infty} f' \cdot e^{-st} dt - f'(0) \\ & = s(sF(s) - f(0)) - f'(0) = s^{2}F(s) - sf(0) - f'(0) \\ & \vdots \\ & \mathfrak{L}\left\{\frac{d^{n}f}{dt^{n}}\right\} = \int_{0}^{\infty} f^{(n)} \cdot e^{-st} dt = f(t)^{(n-1)}e^{-s} \Big|_{0}^{\infty} - \int_{0}^{\infty} f^{(n-1)} \cdot (-s)e^{-st} dt \\ & = s \int_{0}^{\infty} f^{(n-1)} \cdot e^{-s} dt - f^{(n-1)}(0) = s \left(\mathfrak{L}\left\{\frac{d^{n-1}f}{dt^{n-1}}\right\} - f^{(n-1)}(0) \right. \\ & = s^{n}F(s) - s^{n-1}f(0) - \cdots - sf^{(n-2)}(0) - f^{(n-1)}(0) \end{split}$$

CHBE320 Process Dynamics and Control

Korea University 5-11



CHBE320 Process Dynamics and Control

Korea University 5-10

• If $f(0) = f'(0) = f''(0) = \dots = f^{(n-1)}(0) = 0$,

- Initial condition effects are vanished.
- It is very convenient to use deviation variables so that all the effects of initial condition vanish.

$$\mathfrak{L}\left\{\frac{df}{dt}\right\} = sF(s)$$

$$\mathfrak{L}\left\{\frac{d^2f}{dt^2}\right\} = s^2F(s)$$

$$\vdots$$

$$\mathfrak{L}\left\{\frac{d^nf}{dt^n}\right\} = s^nF(s)$$

• Transforms of linear differential equations.

$$y(t) \xrightarrow{\varrho} Y(s), \qquad u(t) \xrightarrow{\varrho} U(s)$$

$$\frac{dy(t)}{dt} \xrightarrow{\varrho} sY(s) \quad (\text{if } y(0) = 0)$$

$$\tau \frac{dy(t)}{dt} = -y(t) + Ku(t) \quad (y(0) = 0) \xrightarrow{\varrho} (\tau s + 1)Y(s) = KU(s)$$

$$\frac{\partial T_L}{\partial t} = -v \frac{\partial T_L}{\partial z} + \frac{1}{\tau_{HL}} (T_w - T_L) \stackrel{\mathfrak{L}}{\longrightarrow} \tau_{HL} v \frac{\partial \widetilde{T}_L(s)}{\partial z} + (\tau_{HL} s + 1) \widetilde{T}_L(s) = \widetilde{T}_w(s)$$

CHBE320 Process Dynamics and Control

Integration

$$\begin{split} \mathfrak{L}\left\{\int_{0}^{t}f(\xi)d\xi\right\} &= \int_{0}^{\infty}\left(\int_{0}^{t}f(\xi)d\xi\right)e^{-st}dt \\ &= \frac{e^{-s}}{-s}\int_{0}^{t}f(\xi)dt\bigg|_{0}^{\infty}\frac{\mathbf{1}}{t}+\frac{1}{s}\int_{0}^{\infty}f\cdot e^{-st}dt = \frac{F(s)}{s} \qquad \text{(by } i. \ b. \ p. \text{)} \\ &\left(\text{Leibniz rule: } \frac{d}{dt}\int_{a(t)}^{b(t)}f(\tau)d\tau = f(b(t))\frac{db(t)}{dt}-f(a(t))\frac{da(t)}{dt}\right) \end{split}$$

• Time delay (Translation in time)

Time delay (Translation in time)
$$f(t) \xrightarrow{+\theta \text{ in}t} f(t-\theta)S(t-\theta)$$

$$\mathfrak{L}\{f(t-\theta)S(t-\theta)\} = \int_{0}^{\infty} f(t-\theta)e^{-st}dt = \int_{0}^{\infty} f(\tau)e^{-s(\tau+\theta)}d\tau \quad (\text{let } \tau = t-\theta)$$

 $= e^{-\theta} \int_{-\infty}^{\infty} f(\tau)e^{-\tau s} d\tau = e^{-\theta} F(s)$

Derivative of Laplace transform

$$\frac{dF(s)}{ds} = \frac{d}{ds} \int_0^\infty f \cdot e^{-s} dt = \int_0^\infty f \cdot \frac{d}{ds} e^{-s} dt = \int_0^\infty (-t \cdot f) e^{-s} dt = \mathfrak{L}[-t \cdot f(t)]$$

CHBE320 Process Dynamics and Control

Korea University 5-13

EXAMPLE ON LAPLACE TRANSFORM (1)

$$f(t) = \begin{cases} 1.5t & \text{for } 0 \le t < 2\\ 3 & \text{for } 2 \le t < 6\\ 0 & \text{for } 6 \le t\\ 0 & \text{for } t < 0 \end{cases}$$

$$f(t) = 1.5t S(t) - 1.5(t-2) S(t-2) - 3 S(t-6)$$

$$\therefore F(s) = \mathfrak{L}{f(t)} = \frac{1.5}{s^2} (1 - e^{-2}) - \frac{3}{s} e^{-6s}$$

• For $F(s) = \frac{2}{s-5}$, find f(0) and $f(\infty)$.

- Using the initial and final value theorems

$$f(0) = \lim_{s \to \infty} s F(s) = \lim_{s \to \infty} \frac{2s}{s - 5} = 2 \qquad f(\infty) = \lim_{s \to 0} s F(s) = \lim_{s \to 0} \frac{2s}{s - 5} = 0$$

- But the final value theorem is not valid because

$$\lim_{t \to \infty} f(t) = \lim_{t \to \infty} 2e^{5t}$$

CHBE320 Process-Dymamics and Control

Korea University 5-15

Final value theorem

From the LT of differentiation, as s approaches to zero

$$\lim_{s \to 0} \int_0^\infty \frac{df}{dt} \cdot e^{-st} dt = \int_0^\infty \frac{df}{dt} \cdot \lim_{s \to 0} e^{-st} dt = \lim_{s \to 0} [sF(s) - f(0)]$$

$$\int_0^\infty \frac{df}{dt} dt = f(\infty) - f(0) = \lim_{s \to 0} sF(s) - f(0) \Rightarrow f(\infty) = \lim_{s \to 0} sF(s)$$

– Limitation: $f(\infty)$ has to exist. If it diverges or oscillates, this theorem is not valid.

Initial value theorem

From the LT of differentiation, as s approaches to infinity

$$\lim_{s \to \infty} \int_0^\infty \frac{df}{dt} \cdot e^{-st} dt = \lim_{s \to \infty} [sF(s) - f(0)]$$

$$\lim_{s \to \infty} \int_0^\infty \frac{df}{dt} e^{-s} dt = 0 = \lim_{s \to \infty} sF(s) - f(0) \Rightarrow f(0) = \lim_{s \to \infty} sF(s)$$

CHBE320 Process Dynamics and Control

Korea University 5-14

EXAMPLE ON LAPLACE TRANSFORM (2)

What is the final value of the following system?

$$x'' + x' + x = \sin t; \ x(0) = x'(0) = 0$$

$$\Rightarrow s^2 X(s) + sX(s) + X = \frac{1}{s^2 + 1} \Rightarrow x(s) = \frac{1}{(s^2 + 1)(s^2 + s + 1)}$$

$$x(\infty) = \lim_{s \to 0} \frac{s}{(s^2 + 1)(s^2 + s + 1)} = 0$$

- Actually, $\chi(\infty)$ cannot be defined due to sin t term.
- Find the Laplace transform for $(t \sin \omega t)$?

From
$$\frac{dF(s)}{ds} = \mathfrak{L}[-t \cdot f(t)]$$

$$\mathfrak{L}[t \cdot \sin \omega t] = -\frac{d}{ds} \left[\frac{\omega}{c^2 + \omega^2} \right] = \frac{2\omega s}{(c^2 + \omega^2)^2}$$

CHBE320 Process Dynamics and Control

INVERSE LAPLACE TRANSFORM

Used to recover the solution in time domain

$$\mathfrak{L}^{-1}{F(s)} = f(t)$$

- From the table
- By partial fraction expansion
- By inversion using contour integral

$$f(t) = \mathfrak{L}^{-1}{F(s)} = \frac{1}{2\pi j} \oint_{\mathcal{C}} e^{st} F(s) ds$$

- Partial fraction expansion
 - After the partial fraction expansion, it requires to know some simple formula of inverse Laplace transform such as

$$\frac{1}{(\tau s+1)}, \frac{s}{(s+b)^2 + \omega^2}, \frac{(n-1)!}{s^n}, \frac{e^{-\theta s}}{\tau^2 s^2 + 2\zeta \tau s + 1}, \text{ etc.}$$

CHBE320 Process Dynamics and Control

Korea University 5-17

· Case II: Some roots are repeated

$$F(s) = \frac{N(s)}{D(s)} = \frac{N(s)}{(s+p)^r} = \frac{b_{r-1}s^{r-1} + \dots + b_0}{(s+p)^r} = \frac{\alpha_1}{(s+p)} + \dots + \frac{\alpha_r}{(s+p)^r}$$

- Each repeated factors have to be separated first.
- Same methods as Case I can be applied.
- Heaviside expansion for repeated factors

$$\alpha_{r-i} = \frac{1}{i!} \frac{d^{(i)}}{ds^{(i)}} \left(\frac{N(s)}{D(s)} (s+p)^r \right) \bigg|_{s=-n} (i=0, \dots, r-1)$$

- Inverse LT

$$f(t) = \alpha_1 e^{-p} + \alpha_2 t e^{-pt} + \dots + \frac{\alpha_r}{(r-1)!} t^{r-1} e^{-pt}$$

PARTIAL FRACTION EXPANSION

$$F(s) = \frac{N(s)}{D(s)} = \frac{N(s)}{(s+p_1)\cdots(s+p_n)} = \frac{\alpha_1}{(s+p_1)} + \dots + \frac{\alpha_n}{(s+p_n)}$$

- Case I: All p_i's are distinct and real
 - By a root-finding technique, find all roots (time-consuming)
 - Find the coefficients for each fraction
 - · Comparison of the coefficients after multiplying the denominator
 - Replace some values for s and solve linear algebraic equation
 - · Use of Heaviside expansion
 - Multiply both side by a factor, $(s+p_i)$, and replace s with $-p_i$.

$$\alpha_i = (s + p_i) \frac{N(s)}{D(s)} \Big|_{s = -p_i}$$

- Inverse LT:

$$f(t) = \alpha_1 e^{-p_1 t} + \alpha_2 e^{-p_2 t} + \dots + \alpha_n e^{-p_n t}$$

CHBE320 Process Dynamics and Control

Korea University 5-18

• Case III: Some roots are complex

$$F(s) = \frac{N(s)}{D(s)} = \frac{c_1 s + c_0}{s^2 + d_1 s + d_0} = \frac{\alpha_1(s+b) + \beta_1 \omega}{(s+b)^2 + \omega^2}$$

- Each repeated factors have to be separated first.
- Then,

$$\frac{\alpha_1(s+b) + \beta_1 \omega}{(s+b)^2 + \omega^2} = \alpha_1 \frac{(s+b)}{(s+b)^2 + \omega^2} + \beta_1 \frac{\omega}{(s+b)^2 + \omega^2}$$

where
$$b = d_1/2$$
, $\omega = \sqrt{d_0 - {d_1}^2/4}$
 $\alpha_1 = c_1$, $\beta_1 = (c_0 - \alpha_1 b)/\omega$

- Inverse LT

$$f(t) = \alpha_1 e^{-bt} \cos \omega \, t + \beta_1 e^{-b} \sin \omega \, t$$

EXAMPLES ON INVERSE LAPLACE TRANSFORM

•
$$F(s) = \frac{(s+5)}{s(s+1)(s+2)(s+3)} = \frac{A}{s} + \frac{B}{s+1} + \frac{C}{s+2} + \frac{D}{s+3}$$
 (distinct)

Multiply each factor and insert the zero value

$$\frac{(s+5)}{(s+1)(s+2)(s+3)}\bigg|_{s=0} = \left(A + s \frac{B}{s+1} + s \frac{C}{s+2} + s \frac{D}{s+3}\right)\bigg|_{s=0} \Rightarrow A = 5/6$$

$$\frac{(s+5)}{s(s+2)(s+3)}\bigg|_{s=-1} = \left(\frac{A(s+1)}{s} + B + \frac{C(s+1)}{s+2} + \frac{D(s+1)}{s+3}\right)\bigg|_{s=-1} \Rightarrow B = -2$$

$$\frac{(s+5)}{s(s+1)(s+3)}\bigg|_{s=-2} = \left(\frac{A(s+2)}{s} + \frac{B(s+2)}{s+1} + C + \frac{D(s+2)}{s+3}\right)\bigg|_{s=-2} \Rightarrow C = 3/2$$

$$\frac{(s+5)}{s(s+1)(s+2)}\bigg|_{s=-3} = \left(\frac{A(s+3)}{s} + \frac{B(s+3)}{s+1} + \frac{C(s+3)}{s+2} + D\right)\bigg|_{s=-3} \Rightarrow D = -1/3$$

$$\therefore f(t) = \Re^{-1}\{F(s)\} = \frac{5}{6} - 2e^{-t} + \frac{3}{2}e^{-2t} - \frac{1}{3}e^{-3}$$

CHBE320 Process Dynamics and Control

CHBE320 Process Dynamics and Control

Korea University 5-21

•
$$F(s) = \frac{(s+1)}{s^2(s^2+4s+5)} = \frac{A(s+2)+B}{(s+2)^2+1} + \frac{Cs+D}{s^2}$$
 (complex)
 $s+1 = A(s+2)s^2+Bs^2+(Cs+D)(s^2+4s+5)$
 $= (A+C)s^3+(2A+B+4C+D)s^2+(5C+4D)s+5D$
 $\therefore A = -C, \quad 2A+B+4C+D = 0, \quad 5C+4D = 1, \quad 5D = 1$
 $\Rightarrow A = -1/25, \quad B = -7/25, \quad C = 1/25, \quad D = 1/5$
 $\frac{A(s+2)+B}{(s+2)^2+1} = -\frac{1}{25}\frac{(s+2)}{(s+2)^2+1} - \frac{7}{25}\frac{B}{(s+2)^2+1}$
 $\frac{Cs+D}{s^2} = \frac{1}{25}\frac{1}{s} + \frac{1}{5}\frac{1}{s^2}$
 $\therefore f(t) = \mathfrak{L}^{-1}{F(s)} = -\frac{1}{25}e^{-2}\cos t - \frac{7}{25}e^{-2}\sin t + \frac{1}{25} + \frac{1}{5}t$

Korea University 5-23

•
$$F(s) = \frac{1}{(s+1)^3(s+2)} = \frac{As^2 + Bs + C}{(s+1)^3} + \frac{D}{(s+2)}$$
 (repeated)

$$1 = (As^2 + Bs + C)(s+2) + D(s+1)^3$$

$$= (A+D)s^3 + (2A+B+3D)s^2 + (2B+C+3D)s + (2C+D)$$

$$\therefore A = -D, \quad 2A+B+3D = 0, \quad 2B+C+3D = 0, \quad 2C+D = 1$$

$$\Rightarrow A = 1, \quad B = 1, \quad C = 1, \quad D = -1$$

$$- \text{ Use of Heaviside expansion} \quad \alpha_{r-i} = \frac{1}{i!} \frac{d^{(i)}}{ds^{(i)}} \left(\frac{N(s)}{D(s)} (s+p)^r \right) \Big|_{s=-p} \quad (i = 0, \dots, r-1)$$

$$\frac{s^2 + s + 1}{(s+1)^3} = \frac{\alpha_1}{(s+1)} + \frac{\alpha_2}{(s+1)^2} + \frac{\alpha_3}{(s+1)^3}$$

$$(i = 0): \alpha_3 = (s^2 + s + 1) \Big|_{s=-1} = 1$$

$$(i = 1): \alpha_2 = \frac{1}{1!} \frac{d}{ds} (s^2 + s + 1) \Big|_{s=-1} = -1$$

$$(i = 2): \alpha_1 = \frac{1}{2!} \frac{d^2}{ds^2} (s^2 + s + 1) \Big|_{s=-1} = 1$$

$$\therefore f(t) = \mathfrak{L}^{-1} \{F(s)\} = e^{-t} - te^{-t} + \frac{1}{2} t^2 e^{-t} - e^{-2t}$$

CHBE320 Process Dynamics and Control

Korea University 5-22

•
$$F(s) = \frac{1 + e^{-2s}}{(4s+1)(3s+1)} = \left(\frac{A}{4s+1} + \frac{B}{3s+1}\right)(1 + e^{-2})$$
 (Time delay)

$$A = 1/(3s+1)\Big|_{s=-1/4} = 4, \qquad B = 1/(4s+1)\Big|_{s=-1/3} = -3$$

$$\therefore f(t) = \mathfrak{L}^{-1}{F(s)} = \mathfrak{L}^{-1}\left\{\frac{4}{4s+1} - \frac{3}{3s+1}\right\} + \mathfrak{L}^{-1}\left\{\frac{4e^{-2s}}{4s+1} - \frac{3e^{-2s}}{3s+1}\right\}$$

$$= e^{-t/4} - e^{-t/3} + \left(e^{-(t-2)/4} - e^{-(t-2)/3}\right)S(t-2)$$



CHBE320 Process Dynamics and Control

SOLVING ODE BY LAPLACE TRANSFORM

Procedure

- 1. Given linear ODE with initial condition,
- 2. Take Laplace transform and solve for output
- 3. Inverse Laplace transform

• **Example:** Solve for
$$5\frac{dy}{dt} + 4y = 2$$
; $y(0) = 1$

$$\mathfrak{L}\left\{5\frac{dy}{dt}\right\} + \mathfrak{L}\left\{4y\right\} = \mathfrak{L}\left\{2\right\} \ \Rightarrow \ 5(sY(s) - y(0)) + 4Y(s) = \frac{2}{s}$$

$$(5s+4)Y(s) = \frac{2}{s} + 5 \implies Y(s) = \frac{5s+2}{s(5s+4)}$$

$$\therefore y(t) = \mathfrak{L}^{-1}\{Y(s)\} = \mathfrak{L}^{-1}\left\{\frac{0.5}{s} + \frac{2.5}{5s + 4}\right\} = 0.5 + 0.5e^{-0.8t}$$

CHBE320 Process Dynamics and Control

Korea University 5-25

TRANSFER FUNCTION (2)

Benefits

Once TF is known, the output response to various given inputs can be obtained easily.

$$y(t) = \mathfrak{L}^{-1}\{Y(s)\} = \mathfrak{L}^{-1}\{G(s)U(s)\} \neq \mathfrak{L}^{-1}\{G(s)\}\mathfrak{L}^{-1}\{U(s)\}$$

- Interconnected system can be analyzed easily.
 - · By block diagram algebra

$$X \leftarrow G1 \qquad G2 \qquad Y \leftarrow X(s) = \frac{G1(s)G2(s)}{1 + G1(s)G2(s)G3(s)}$$

- Easy to analyze the qualitative behavior of a process, such as stability, speed of response, oscillation, etc.
 - · By inspecting "Poles" and "Zeros"
 - Poles: all s's satisfying D(s)=0
 - Zeros: all s's satisfying N(s)=0

CHBE320 Process Dynamics and Control Korea University 5-27

TRANSFER FUNCTION (1)

Definition

 An algebraic expression for the dynamic relation between the input and output of the process model

$$5\frac{dy}{dt} + 4y = u; \ y(0) = 1$$
Let $\tilde{y} = y - 1$ and $\tilde{u} = u - 4$

$$(5s + 4)\tilde{Y}(s) = \tilde{U}(s) \Rightarrow \frac{\tilde{Y}(s)}{\tilde{U}(s)} = \frac{1}{5s + 4} = 0.25$$

$$0.25$$

$$1.25s + 1$$

$$0.5s + 4$$

- How to find transfer function
 - 1. Find the equilibrium point
 - 2. If the system is nonlinear, then linearize around equil. point
 - 3. Introduce deviation variables
 - 4. Take Laplace transform and solve for output
 - 5. Do the Inverse Laplace transform and recover the original variables from deviation variables

CHBE320 Process Dynamics and Control

Korea University 5-26

TRANSFER FUNCTION (3)

 Steady-state Gain: The ratio between ultimate changes in input and output

Gain=
$$K = \frac{\Delta \text{ouput}}{\Delta \text{input}} = \frac{(y(\infty) - y(0))}{(u(\infty) - u(0))}$$

- For a unit step change in input, the gain is the change in output
- Gain may not be definable: for example, integrating processes and processes with sustaining oscillation in output
- From the final value theorem, unit step change in input with zero initial condition gives

$$K = \frac{y(\infty)}{1} = \lim_{s \to 0} s \, Y(s) = \lim_{s \to 0} s \, G(s) \frac{1}{s} = \lim_{s \to 0} G(s)$$

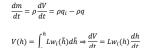
- The transfer function itself is an impulse response of the

system $Y(s) = G(s)U(s) = G(s)\mathfrak{L}\{\delta(t)\} = G(s)$

CHBE320 Process Dynamics and Control

EXAMPLE

Horizontal cylindrical storage tank (Ex4.7)





$$w_i(h)/2 = \sqrt{R^2 - (R-h)^2} = \sqrt{(2R-h)h}$$

$$w_l L \frac{dh}{dt} = q_l - q \implies \frac{dh}{dt} = \frac{1}{2L\sqrt{(D-h)h}}(q_l - q)$$
 (Nonlinear ODE)

- Equilibrium point: $(\bar{q}_i, \bar{q}, \bar{h})$ $0 = (\bar{q}_i \bar{q})/(2L\sqrt{(D \bar{h})\bar{h}})$ (if $\bar{q}_i = \bar{q}$, \bar{h} can be any value in $0 \le \bar{h} \le D$.)
- Linearization:

$$\frac{dh}{dt} = f(h,q_l,q) = \frac{\partial f}{\partial h} \bigg|_{(\tilde{h},\tilde{q}_l,\tilde{q})} (h-\tilde{h}) + \frac{\partial f}{\partial q_l} \bigg|_{(\tilde{h},\tilde{q}_l,\tilde{q})} (q_l-\tilde{q}_l) + \frac{\partial f}{\partial q} \bigg|_{(\tilde{h},\tilde{q}_l,\tilde{q})} (q-\bar{q})$$

CHBE320 Process Dynamics and Control

Korea University 5-29

PROPERTIES OF TRANSFER FUNCTION

Additive property

$$Y(s) = Y_1(s) + Y_2(s)$$

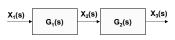
= $G_1(s)X_1(s) + G_2(s)X_2(s)$



· Multiplicative property

$$X_3(s) = G_2(s)X_2(s)$$

= $G_2(s)[G_1(s)X_1(s)]$



Physical realizability

CHBE320 Process Dynamics and Control

- In a transfer function, the order of numerator(m) is greater than that of denominator(n): called "physically unrealizable"
- The order of derivative for the input is higher than that of output. (requires future input values for current output)

Korea University 5-31

$$\begin{aligned} \frac{\partial f}{\partial h} \bigg|_{(\tilde{h},\tilde{q}_l,\tilde{q})} &= (\tilde{q}_l - \tilde{q}) \frac{\partial}{\partial h} \frac{-1}{2L\sqrt{(D-h)h}} = 0 \quad (\because \tilde{q}_l = \tilde{q}) \\ \frac{\partial f}{\partial q} \bigg|_{(\tilde{h},\tilde{q}_l,\tilde{q})} &= \frac{-1}{2L\sqrt{(D-\tilde{h})\tilde{h}}}, \qquad \frac{\partial f}{\partial q_l} \bigg|_{(\tilde{h},\tilde{q}_l,\tilde{q})} = \underbrace{\frac{1}{2L\sqrt{(D-\tilde{h})\tilde{h}}}} \end{aligned}$$

$$s\widetilde{H}(s) = k\widetilde{Q}_i(s) - k\widetilde{Q}(s)$$

- Transfer function between $\widetilde{H}(s)$ and $\widetilde{Q}(s)$: $-\frac{k}{s}$ (integrating)
- Transfer function between $\overline{\widetilde{H}(s) \text{ and } \widetilde{Q}_i(s): \frac{k}{s}}$ (integrating)
- If ħ is near 0 or D, k becomes very large and ħ is around D/2, k becomes minimum.
- ⇒ The model could be quite different depending on the operating condition used for the linearization.
- ⇒ The best suitable range for the linearization in this case is around D/2. (less change in gain)
- ⇒ Linearized model would be valid in very narrow range near 0.

CHBE320 Process Dynamics and Control

Korea University 5-30

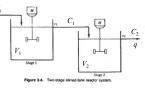
EXAMPLES ON TWO TANK SYSTEM

• Two tanks in series (Ex3.7) $\underline{\varsigma}$

- No reaction

$$V_1 \frac{dc_1}{dt} + qc_1 = qc_i$$

$$V_2 \frac{dc_2}{dt} + qc_2 = qc_1$$



- Initial condition: $c_1(0) = c_2(0) = 1 \text{ kg mol/m}^3$ (Use deviation var.)
- Parameters: $V_1/q=2$ min., $V_2/q=1.5$ min.
- Transfer functions

$$\frac{\tilde{C}_1(s)}{\tilde{C}_i(s)} = \frac{1}{(V_1/q)s + 1} \qquad \qquad \frac{\tilde{C}_2(s)}{\tilde{C}_1(s)} = \frac{1}{(V_2/q)s + 1}$$

$$\frac{\tilde{\mathcal{C}}_2(s)}{\tilde{\mathcal{C}}_i(s)} = \frac{\tilde{\mathcal{C}}_2(s)}{\tilde{\mathcal{C}}_1(s)} \frac{\tilde{\mathcal{C}}_1(s)}{\tilde{\mathcal{C}}_i(s)} = \frac{1}{((V_2/q)s+1)((V_1/q)s+1)}$$

CHBE320 Process Dynamics and Control

$$\tilde{C}_i^P(s) = \frac{5}{s}(1 - e^{-0.25s})$$

$$\begin{array}{c|c}
\tilde{c}_i^P \\
5 \\
\hline
0.25 \\
t
\end{array}$$

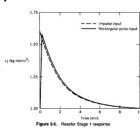
• Equivalent impulse input

$$\tilde{C}_i^{\delta}(s) = \mathfrak{L}\{(5 \times 0.25)\delta(t)\} = 1.25$$

· Pulse response vs. Impulse response

$$\bar{C}_1^P(s) = \frac{1}{2s+1} \bar{C}_i^P(s) = \frac{5}{s(2s+1)} (1 - e^{-0.25s})
= \left(\frac{5}{s} - \frac{10}{2s+1}\right) (1 - e^{-0.25s})
\Rightarrow \bar{c}_1^P(t) = 5(1 - e^{-t/2})
-5(1 - e^{-(t-0.25)/2}) S(t - 0.25)$$

$$\tilde{C}_1^{\delta}(s) = \frac{1}{2s+1} \tilde{C}_i^{\delta}(s) = \frac{1.25}{(2s+1)}$$
$$\Rightarrow \begin{bmatrix} \tilde{c}_1^{\delta} = 0.625e^{-t/2} \end{bmatrix}$$



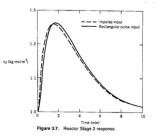
CHBE320 Process Dynamics and Control

Korea University 5-33

$$\tilde{C}_{2}^{P}(s) = \frac{1}{(2s+1)(1.5s+1)} \tilde{C}_{i}^{P}(s) = \frac{5}{s(2s+1)(1.5s+1)} (1 - e^{-0.25s})$$
$$= \left(\frac{5}{s} - \frac{40}{2s+1} + \frac{22.5}{1.5s+1}\right) (1 - e^{-0.25s})$$

$$\Rightarrow \tilde{c}_{2}^{P}(t) = (5 - 20e^{-t/2} + 15e^{-t/1.5}) - (5 - 20e^{-(t - 0.25)/2} + 15e^{-(t - 0.25)/1.5}) S(t - 0.25)$$

$$\begin{split} \tilde{C}_{2}^{\delta}(s) &= \frac{1}{(2s+1)(1.5s+1)} \tilde{C}_{i}^{\delta}(s) \\ &= \frac{1.25}{(2s+1)(1.5s+1)} \\ &= \frac{5}{2s+1} - \frac{3.75}{1.5s+1} \\ &\Rightarrow \tilde{C}_{2}^{\delta} &= 2.5e^{-t/2} - 2.5e^{-t/1.5} \end{split}$$



CHBE320 Process Dynamics and Control