

TG/DTG studies of Fresh Fishing Net and Waste Fishing Net

Seung -Soo Kim

Department of Environmental Engineering, Donghae University,
119, Jiheung -dong, Donghae, Gangwon, 240 -713, Korea

Department of Environmental Engineering, Donghae University

Introduction

Ocean pollution poses serious environmental problems in Korea

→ Need to treat marine wastes in more environmentally friendly manner

Main composition of marine wastes

→ Waste fishing nets (WFN), waste fishing tackles and waste lopes

▶ Characteristics of marine wastes

→ Floating, deposition and moving on seashore

→ Damage of marine ecosystem, cause of loss in the fishing industry

▶ Fishing nets: production, consignment(1997~2000 yr) [unit : Ton]

| Year | Production | Consignment | Remark |
|------|------------|-------------|--------|
| 1997 | 11,057 | 11,571 | - |
| 1998 | 9,607 | 9,895 | - |
| 1999 | 10,066 | 10,442 | - |
| 2000 | 10,916 | 11,033 | - |

자료 : 통계청, “한국산업통계연보”, 2001, p450

Experimental

- ▶ **Thermogravimetric Analysis**

- Thermogravimetric Analyzer (TGA; Cahn, TG-2171)
- Sample : Fresh Fishing Net(Nylon-6), Waste Fishing Net(Nylon-6)
- Mass : 400 mg
- Heating rates : 0.5~2.0 /min (<500)

- ▶ **Micro-scale tubing reactor**

- Reaction temperature : 440
- Reaction time : 60~100 min

- ▶ **Product Analysis**

- Carbon number distribution : GC (Younglin, M600D)
- FT-IR (Thermo Mattson, 60AR)

Experimental

- ▶ Elemental analysis : fresh fishing nets(FFN), waste fishing nets(WFN)

| | Element (wt%) | | | | | H/C ratio |
|-----|---------------|-------|-------|------|-------|-----------|
| | C | H | N | S | O | |
| FFN | 62.68 | 10.66 | 12.24 | – | 14.42 | 2.04 |
| WFN | 56.28 | 8.86 | 10.92 | 0.05 | 14.83 | 1.89 |

Activation Energy

- ▶ **Conversion: X**

$$X = \frac{W_0 - W_t}{W_0 - W_t} \quad (1)$$

- ▶ **Pyrolysis rate:**

$$\frac{dX}{dt} = k f(X) \quad (2)$$

- ▶ **Reaction constant: k**

$$k = A \exp\left(\frac{-E}{RT}\right) \quad (3)$$

- ▶ **Conversion function: f(X)**

$$f(X) = (1 - X)^n \quad (4)$$

- ▶ **Eq.(3), Eq.(4) → Eq.(2)**

$$\frac{dX}{dt} = A \exp\left(\frac{-E}{RT}\right) (1 - X)^n \quad (5)$$

- ▶ **Take logarithm Eq.(6)**

$$\ln\left(\frac{dX}{dt}\right) = \ln\left[A(1 - X)^n\right] - \frac{E}{R} \frac{1}{T} \quad (6)$$

A : pre-exponential factor (sec⁻¹)

n : reaction order

E : activation energy (kJ/mol)

R : gas constant (8.314Jg/mol K)

T : temperature (K)

t : time (sec)

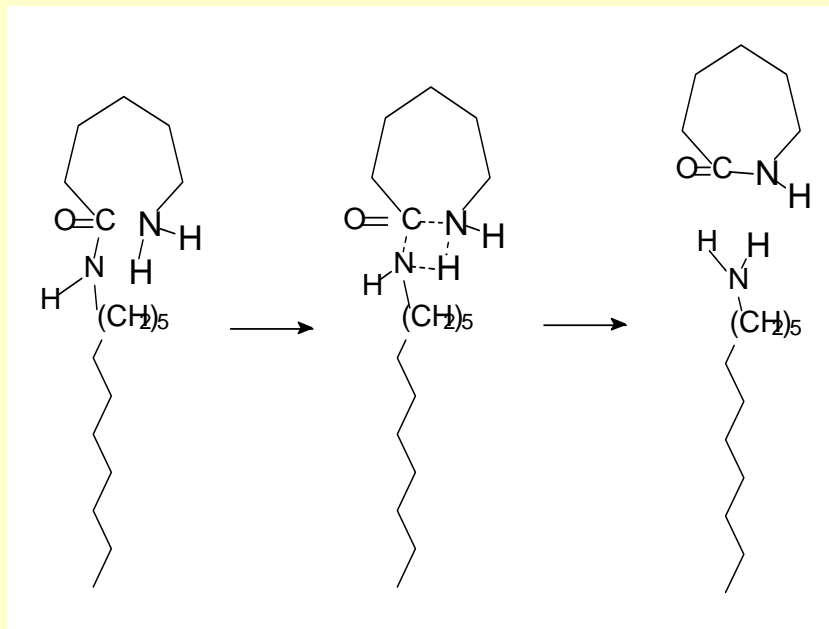
- ▶ **Intercept of Eq.(6) is**

$$\ln\left[A(1 - X)^n\right] = \ln(A) + n \ln(1 - X) \quad (7)$$

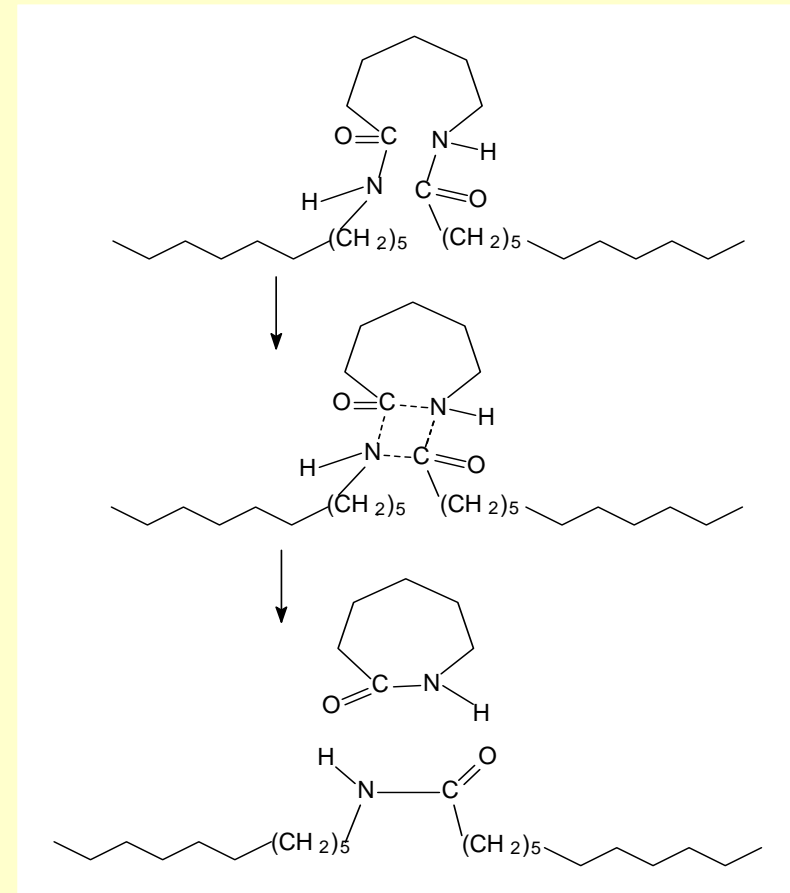
Decomposition mechanism of Nylon -6:

R.S Lehrle et al., *Polymer Degradation and Stability*, **67**, 21(2000)

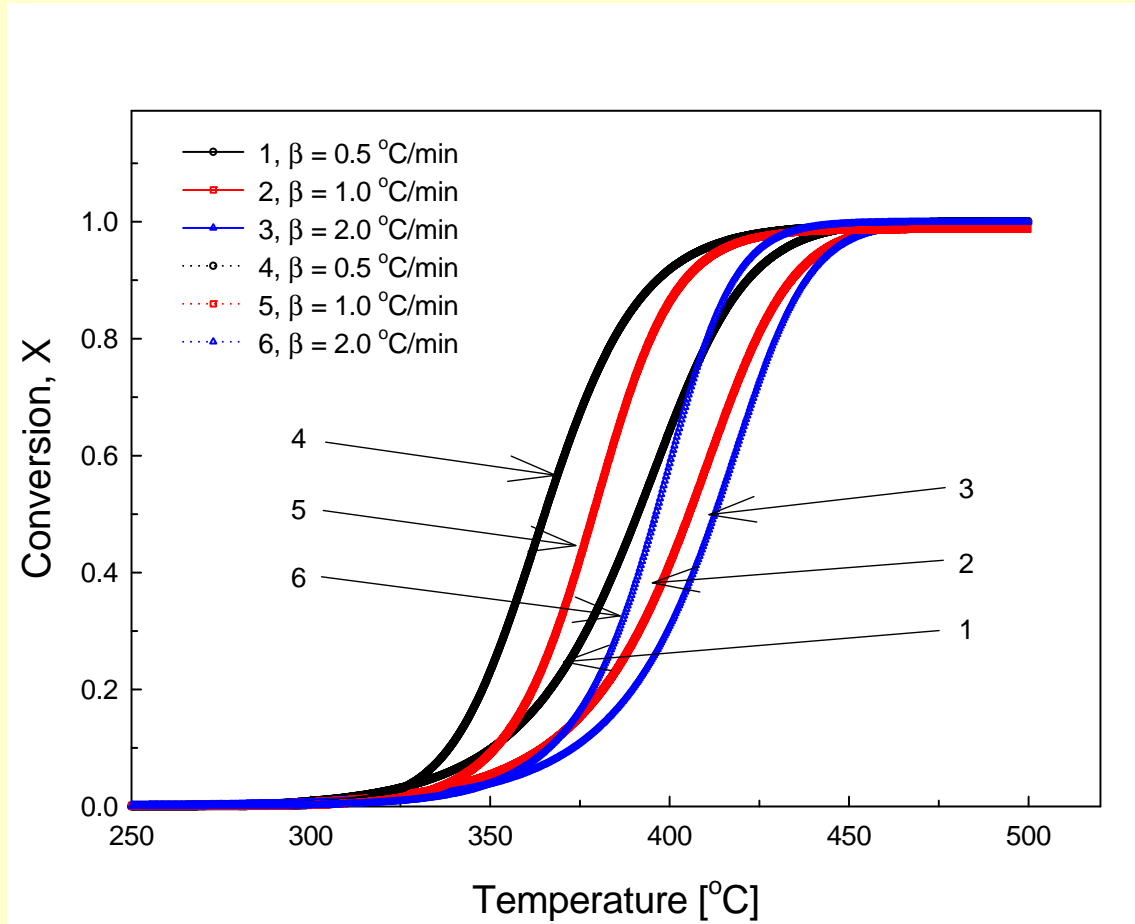
(a) Initial fast rate



(b) Slow rate

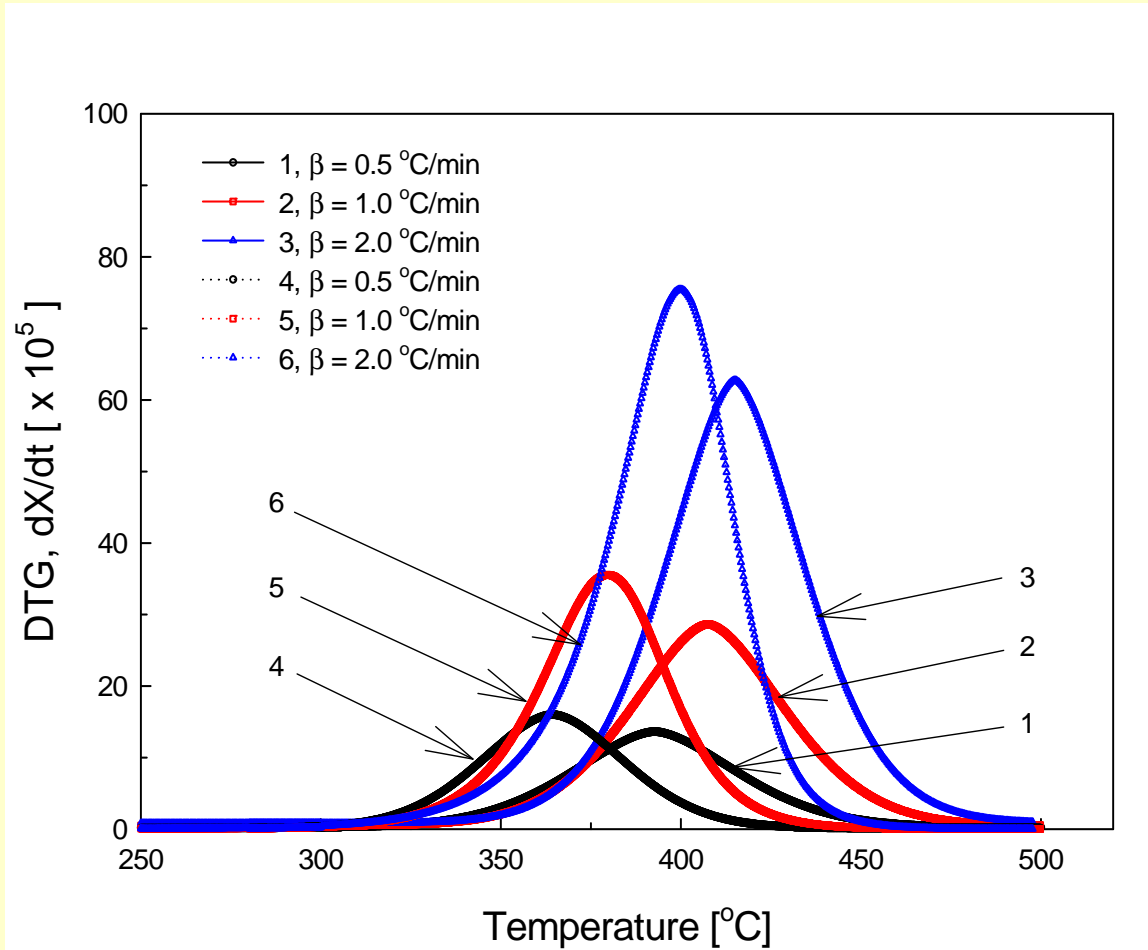


TGA curves : FFN and WFN



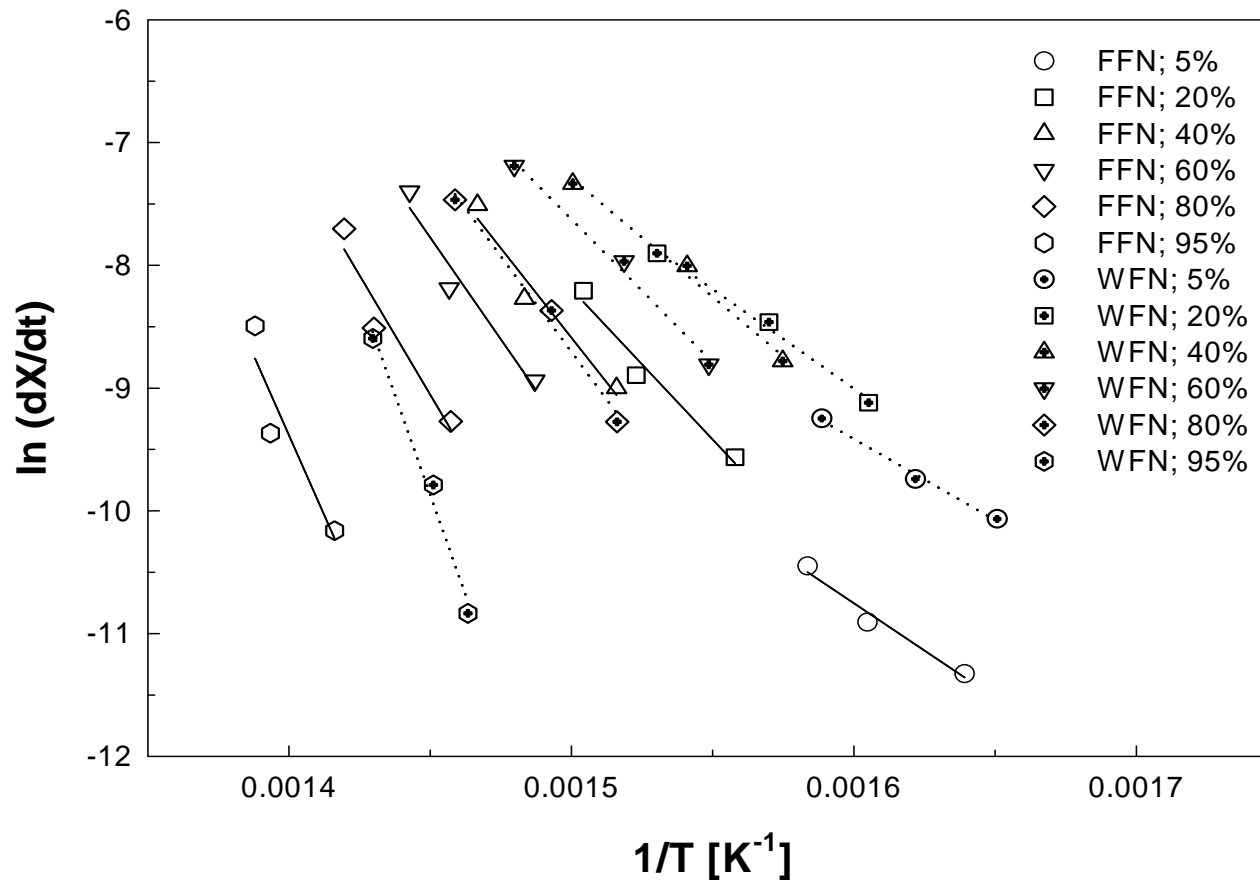
1; FFN; $\beta = 0.5$ /min,
2; FFN; $\beta = 1.0$ /min,
3; FFN; $\beta = 2.0$ /min,
4; WFN; $\beta = 0.5$ /min,
5; WFN; $\beta = 1.0$ /min,
6; WFN; $\beta = 2.0$ /min.

DGT curves : FFN and WFN

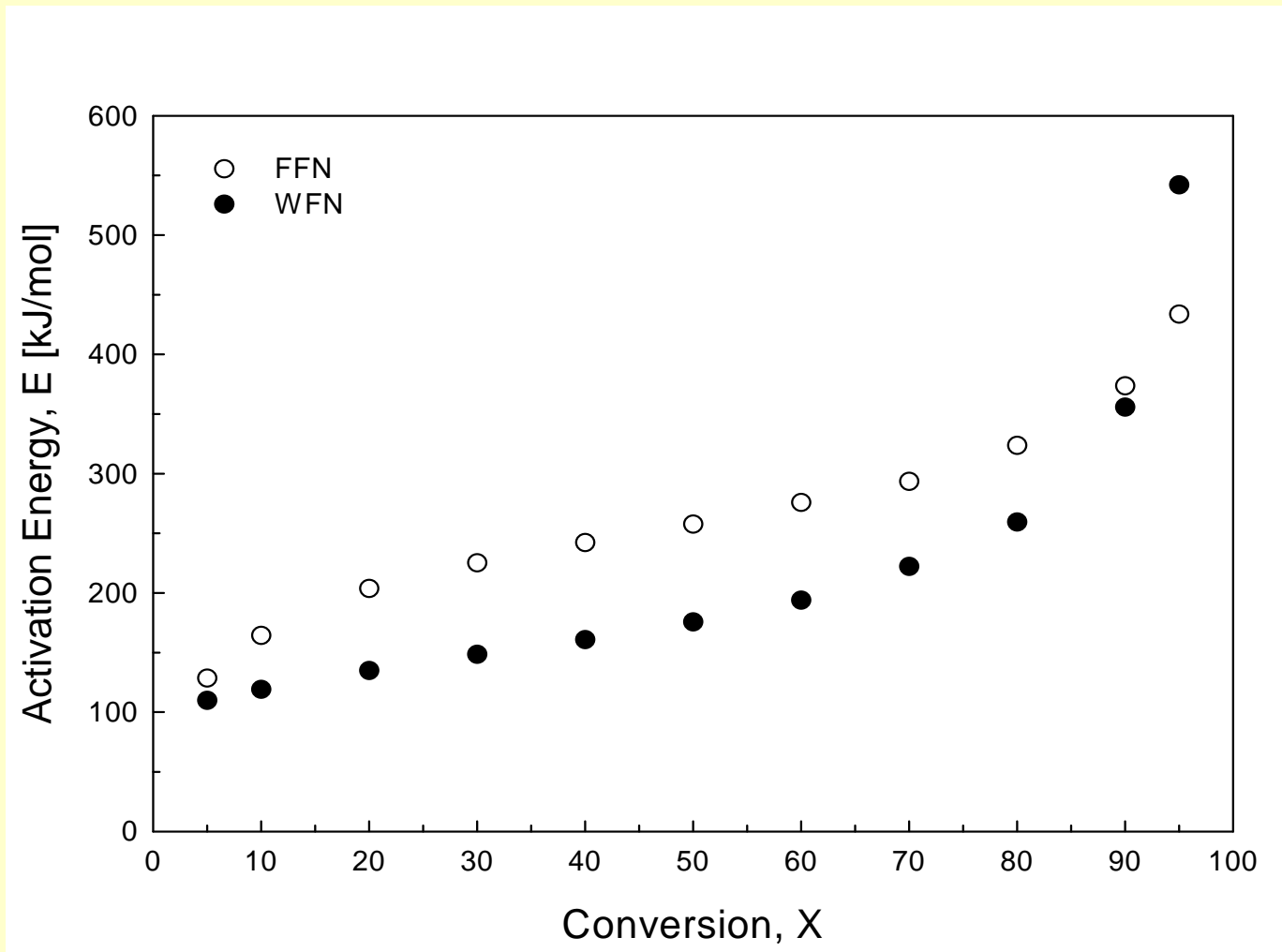


1; FFN; $\beta = 0.5$ /min,
2; FFN; $\beta = 1.0$ /min,
3; FFN; $\beta = 2.0$ /min,
4; WFN; $\beta = 0.5$ /min,
5; WFN; $\beta = 1.0$ /min,
6; WFN; $\beta = 2.0$ /min.

Application of equation 5 : 0.5~2.0 /min



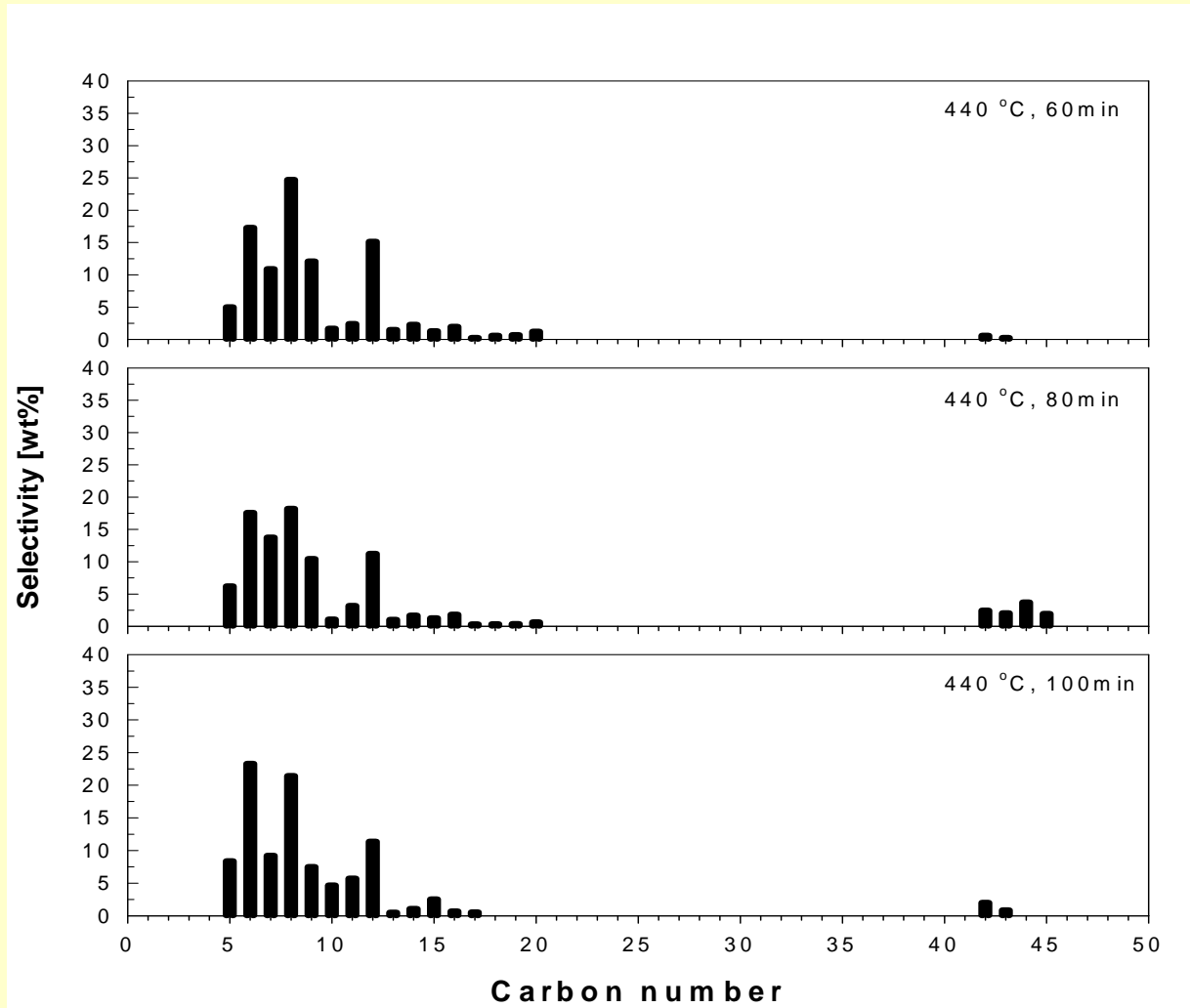
Calculated activation energies



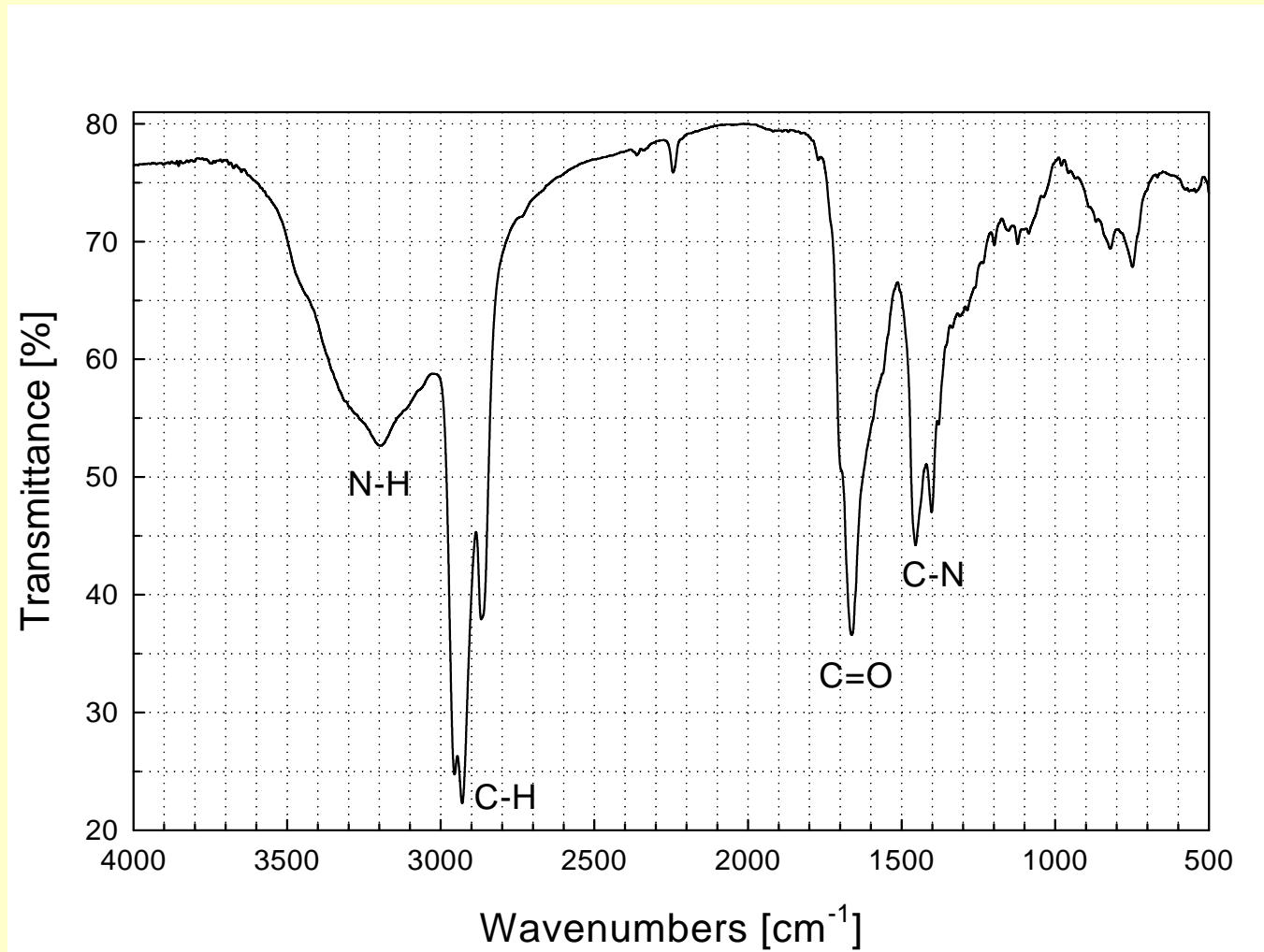
Application of Eq. (7) to calculate pre -exponential factor

| | | Conversion [%] | | | | | | | | | | |
|-----|-----------------|-----------------------|-----------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|--------------------------|
| | | 5 | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 95 |
| FFN | 0 th | 1.17 $\times 10^6$ | 1.57 $\times 10^6$ | 2.45 $\times 10^{12}$ | 1.06 $\times 10^{14}$ | 1.78 $\times 10^{15}$ | 2.03 $\times 10^{16}$ | 3.23 $\times 10^{17}$ | 4.15 $\times 10^{18}$ | 3.74 $\times 10^{20}$ | 5.95 $\times 10^{23}$ | 4.38 $\times 10^{27}$ |
| | 1 st | 1.23 $\times 10^6$ | 1.75 $\times 10^6$ | 3.07 $\times 10^{12}$ | 1.52 $\times 10^{14}$ | 2.96 $\times 10^{15}$ | 4.06 $\times 10^{16}$ | 8.07 $\times 10^{17}$ | 1.38 $\times 10^{19}$ | 1.87 $\times 10^{21}$ | 5.95 $\times 10^{24}$ | 8.76 $\times 10^{28}$ |
| WFN | 0 th | 1.23 $\times 10^5$ | 9.61 $\times 10^5$ | 2.25 $\times 10^7$ | 2.88 $\times 10^8$ | 2.67 $\times 10^9$ | 3.49 $\times 10^{10}$ | 7.58 $\times 10^{11}$ | 8.35 $\times 10^{13}$ | 3.44 $\times 10^{16}$ | 5.39 $\times 10^{23}$ | 5.84 $\times 10^{36}$ |
| | 1 st | 1.29 $\times 10^5$ | 1.07 $\times 10^6$ | 2.82 $\times 10^7$ | 4.12 $\times 10^8$ | 4.46 $\times 10^9$ | 6.98 $\times 10^{10}$ | 1.90 $\times 10^{12}$ | 2.78 $\times 10^{14}$ | 1.72 $\times 10^{17}$ | 2.39 $\times 10^{24}$ | 1.17 $\times 10^{38}$ |

Carbon number distribution : 440 , 60~100 min



IR -spectra for FFN : 440 , 100 min



Conclusion

- ▶ The apparent activation energies increased with an increase of conversion. The average activation energy for **FFN** was **266 kJ mol⁻¹**, while that of **WFN** was **220 kJ mol⁻¹**.
- ▶ Pre-exponential factor was **between 10¹² and 10²¹ sec⁻¹** when the slope of thermogravimetric curves was almost linear.
- ▶ The carbon number of C₆ like caprolactam was slightly increased with the increase of reaction time, but the selectivity of specific hydrocarbons was not observed from the pyrolyzed oil.