

# The Solubility of Carbon Dioxide in Ionic Liquids

(고려대) 최원영, 김용수, 이철수  
(한국기술교육대) 유성식

# Introduction

- Ionic Liquids
  - Organic salts composed of cation and anion
  - Low melting points– near the room temperature
  - Negligible vapor pressure
  - Environmentally favorable solvents
- Motivation
  - Accuracy in equilibrium data is sometimes questioned
  - Few studies have been published on the modeling of equilibria

# Experimental Apparatus

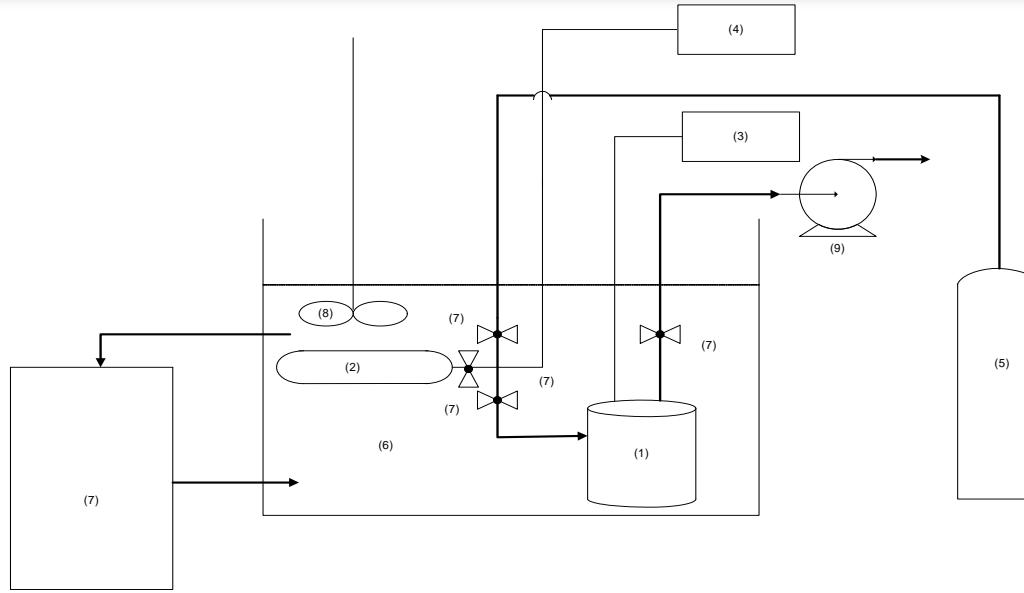


Figure 1. Schematic diagram of experimental apparatus

- (1) equilibrium cell (2)CO<sub>2</sub> storage (3)pressure transducer
- (4) thermocouple (6)water bath (5) CO<sub>2</sub> bomb (7) valve (8) agitator
- (9) vacuum pump (10) circulator

# Experimental

- Procedure
  - Solubilities can be measured as a vapor adsorption on solids
    - ILs have negligible vapor pressure
  - Amount in vapor phase is measured using PVT relation
- Accuracy
  - Temperature
    - Accuracy :  $\pm 0.02\text{K}$
  - Pressure
    - Range :  $0 \sim 10\text{ bar}$  accuracy :  $0.02\text{ bar}$
  - Solubility
    - Mole fraction :  $\pm 0.002$
- Ionic Liquids
  - Amounts of halogen and water less than  $30\text{ppm}$

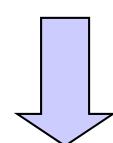
# Model

- Nonrandom Lattice fluid hydrogen-bonding model

(You et al., Fluid Phase Equilib., 93(1994) 193)

(You et al., Fluid Phase Equilib., 93(1994) 194)

- ILs exist as ion-pairs
- The specific interactions such as hydrogen bond did not exist (Haiware et al. J.Fluor.Chem.105(2002) 2437)

  
CO<sub>2</sub>-ILs system can be modeled with physical interactions

# Pure Parameter

- Segment number and interaction energy parameter
  - Parameter determined by using density and vapor pressure
    - For ionic liquids have no detectable vapor pressure

→ assumed that  $P_v < 10^{-5}$  bar

$$\varepsilon_{ii} / k = \varepsilon_a + \varepsilon_b (T - T_0) + \varepsilon_c [T \ln(T_0 / T) + (T - T_0)]$$

$$r_i = r_a + r_b (T - T_0) + r_c [T \ln(T_0 / T) + (T - T_0)]$$

Table 1. Pure parameters for the NLF EOS

species	$\varepsilon_a$	$\varepsilon_b$	$\varepsilon_c$	$r_a$	$r_b$	$r_c$
[bmim][PF <sub>6</sub> ]	126.3448	-0.0387	-3.8358	20.0	0	0
[emim][BF <sub>4</sub> ]	155.0282	-0.2594	0.2810	15.3		
[C <sub>6</sub> mim][BF <sub>4</sub> ]	118.457	0	0	21.0		
CO <sub>2</sub>	84.0970	-0.0977	-0.4073	3.8322	0.0047	0.0053

# Binary parameter

- Interaction between segments of carbon dioxide and ionic liquids

$$\varepsilon_{ij} = (\varepsilon_{ii}\varepsilon_{jj})^{1/2}(1 - \lambda_{ij})$$

$$\lambda_{ij} = \lambda_a + \lambda_b(T - T_0) + \lambda_c[T \ln(T_0/T) + (T - T_0)]$$

Table 2. Binary parameters for the NLF EOS

Species	$\lambda_a$	$\lambda_b$	$\lambda_c$
[bmim] [PF <sub>6</sub> ]	0.0785	6.012×10 <sup>-4</sup>	0.0108
[emim] [BF <sub>4</sub> ]	0.059	0	0
[C <sub>6</sub> mim] [BF <sub>4</sub> ]	-0.017	0	0

# Results

Table 3. Solubility of CO<sub>2</sub> with [C<sub>6</sub>mim][BF<sub>4</sub>] and [emim][BF<sub>4</sub>] at 298.15K

[C <sub>6</sub> mim][BF <sub>4</sub> ]	Mole fraction	[emim][BF <sub>4</sub> ]	Mole fraction
Pressure [bar]		Pressure [bar]	
2.09	0.042	1.62	0.039
2.70	0.053	2.05	0.047
3.19	0.071	2.52	0.056
3.61	0.076	2.95	0.062
3.95	0.081	3.27	0.070
4.43	0.089	3.70	0.076
4.92	0.100	3.99	0.080
5.41	0.109	4.45	0.088
5.88	0.115	4.89	0.097
6.22	0.119	5.39	0.102
6.67	0.127	5.67	0.107
7.11	0.133	5.93	0.111
8.12	0.144	6.39	0.117
		6.73	0.122
		7.15	0.125
		7.46	0.129
		7.96	0.134
		8.45	0.141

# Comparison

Table 4. Comparison of experimental and calculated solubilities

Data ref.	T[K]	P range[bar]	AADx[%]	T[K]	P range[bar]	AADx[%]
[bmim][PF <sub>6</sub> ] 1	293.15	15.33–47.52	3.78	313.15	1.05–94.80	2.58
	333.15	4.24–91.84	1.61	353.15	2.66–96.85	0.94
	373.15	2.29–91.91	0.54	393.15	11.99–83.24	0.34
3	283.15	0.50–12.99	3.00	298.15	0.50–12.99	2.34
	323.15	0.50–12.99	1.43			
2	313.15	15.17–95.67	9.07	323.15	17.38–92.46	11.1
	333.15	15.79–93.01	14.1			
This work	298.15	5.29–6.67	3.02			
[emim][BF <sub>4</sub> ]	298.15	1.62–8.45	0.54			
[C <sub>6</sub> mim][BF <sub>4</sub> ]	298.15	2.09–812	0.31			

1 Kamps et al., J. Chem. Eng. Data, 48(2003) 746

2 Anthony et al., J. Phys. Chem. B, 106(2003) 7315

3 Blanchard et al., J. Phys. Chem. B, 105(2001) 2437

# Discussion

- [Bmim][PF<sub>6</sub>]
  - Solubility data of CO<sub>2</sub> is sometimes questioned
  - The measurement method is very accurate and the error is very likely associated with IL sample
  - Using physical model assuming ion pairs like molecular species obtained good agreements with exception of Blanchard et al.
  - The average deviation between data sets was 5.3% AAD in mole fraction
- [C<sub>6</sub>mim][BF<sub>4</sub>] [Emim][BF<sub>4</sub>]
  - At low pressure, small effect of alkyl chain length was observed

# [BF<sub>4</sub>] System

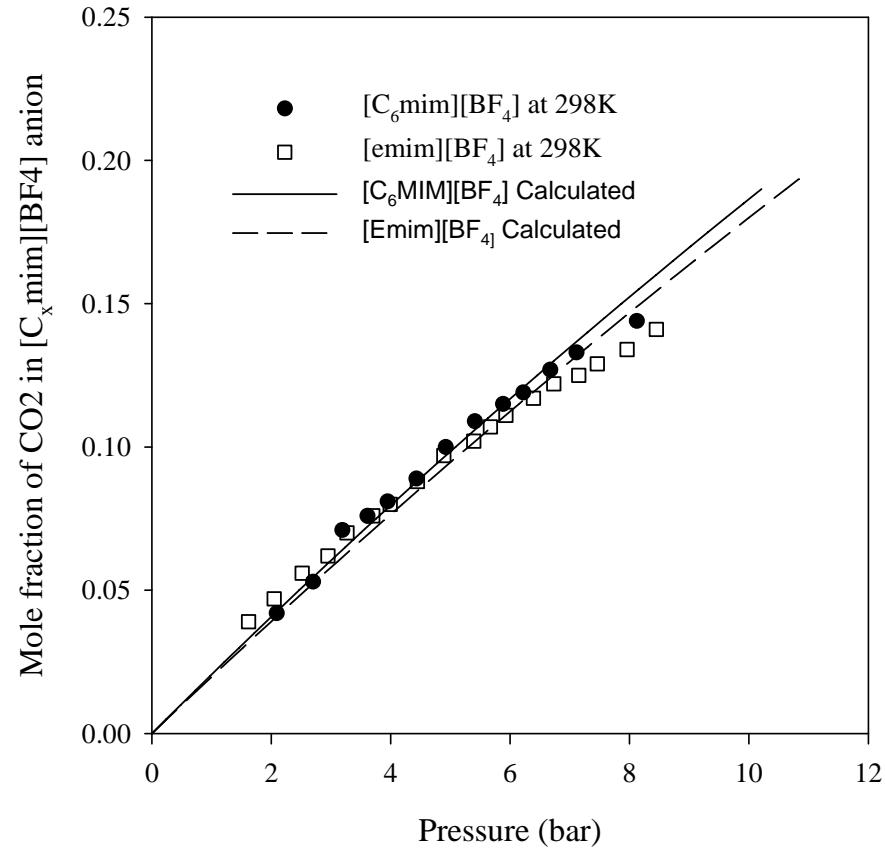


Figure 1. The solubility of carbon dioxide in [Cxmim][BF<sub>4</sub>]

# [PF<sub>6</sub>] System

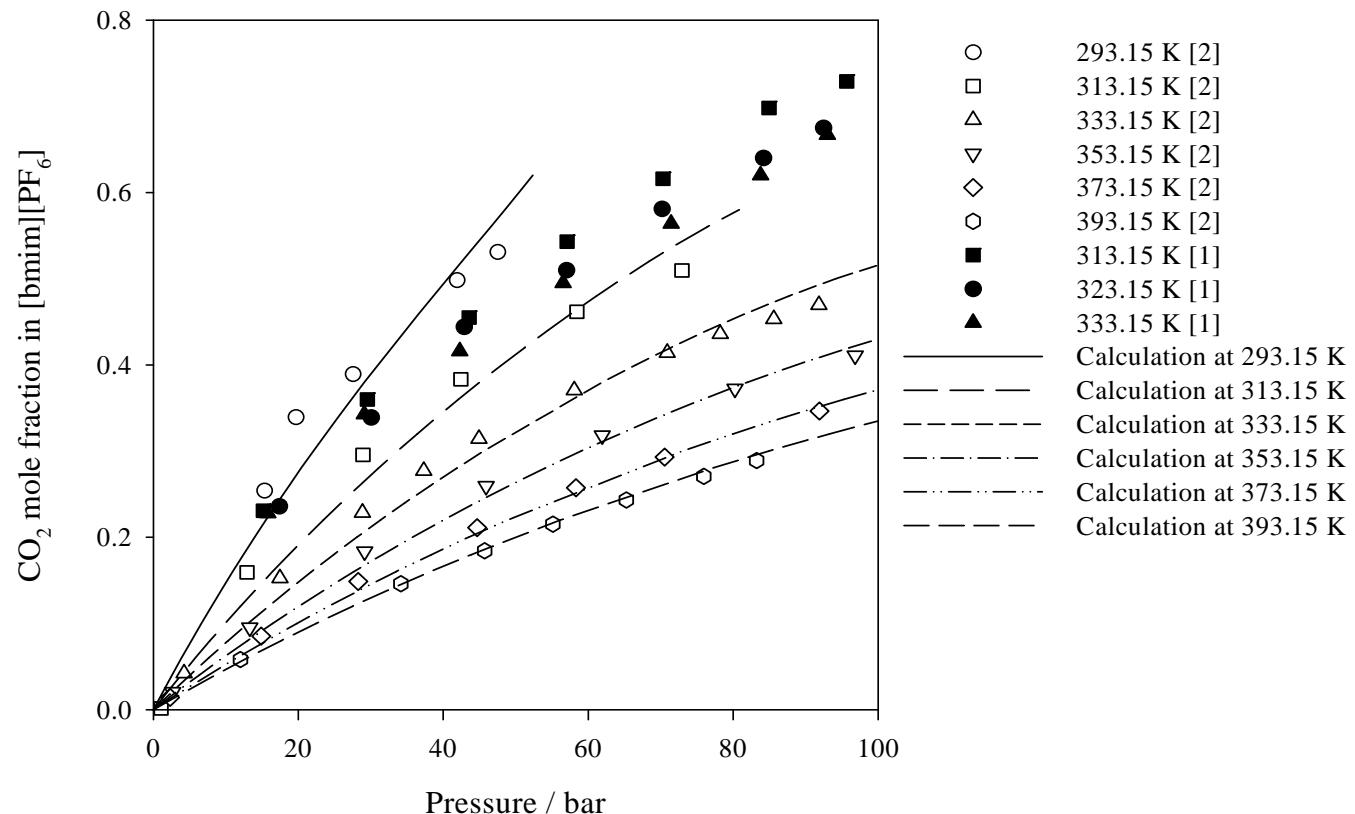


Figure 2. Comparison of the solubility of carbon dioxide in [bmim][PF<sub>6</sub>]

# [PF<sub>6</sub>] System

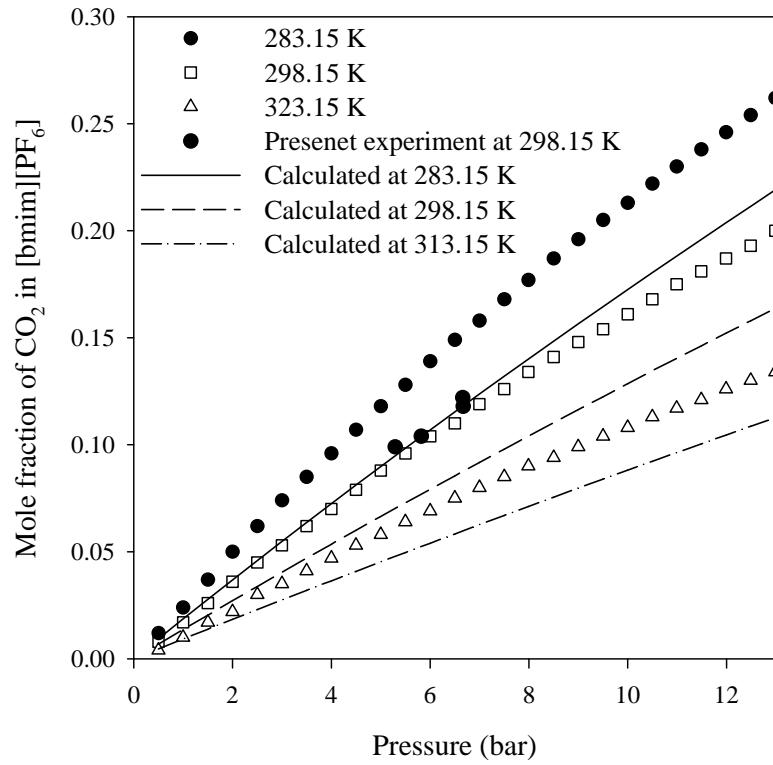


Figure 3. Comparison of the solubility of carbon dioxide in [bmim][PF<sub>6</sub>]

# Conclusion

- The solubility of CO<sub>2</sub> in ionic liquids were experimentally measured
  - [Bmim][PF<sub>6</sub>], [C<sub>6</sub>mim][BF<sub>4</sub>], [Emim][BF<sub>4</sub>]
  - An estimated accuracy is 0.002 mole fraction
- NLF EOS was adopted for phase equilibria of carbon dioxide and ionic liquids
- The calculated results were good with and exception of Blanchard et al.