Optimal Design Method Based On Mp Criteria for Multiloop PID Controllers

Truong Nguyen Luan Vu, Kihong Lee, Moonyong Lee*, Jietae Lee¹

School of Chemical Engineering and Technology, Yeungnam University, ¹Department of Chemical Engineering, Kyungpook National University (mynlee@yu.ac.kr*)

Introduction

Recently, multiloop PID controller is widespread used because of its simple, performance and robustness. The interactions between the control loops are really complicated and correspondingly difficult to make the proper tuning in a MIMO system. For this reason, the proposed method has been used the multiloop diagonal controller's structure for designing multiloop PID controller. In the late 1980s, there were many multiloop PID controller tuning rules which are proposed by the famous authors such as [Luyben, 1986; Grosdidier and Morari, 1987; Skogestad and Morari, 1989; Bassualdo and Marchetti, 1990]. In this article, we propose new tuning rules for multiloop PID controllers to give desired closed-loop responses by an analytical design of multiloop PID controllers. A good combination between diagonal and off-diagonal term in the closed-loop frequency responses that make the interaction effects of the control loop can be adjusted as the desired effect by designer. Considering the process or design goal, it attaches more importance to diagonal or off-diagonal term. In our research, its pair is in equilibrium. The optimum values of closed-loop time constant are found by solving the prososed optimization function. These solutions give the proposed multiloop controllers to minimize integal absolute error (IAE) for all loops. The feasibility of proposed method is verified by several illustrated examples with purpose to show how performance of proposed method, a favorable comparison with some well-known methods.

Theory

1. Proposed Tuning method

1.1. Mp Tuning Criterion for the Multiloop Controllers Tuning

In MIMO system, the closed-loop transfer function can be given by:

$$H(s) = G(s)G_{c}(s)[I + G(s)G_{c}(s)]^{-1}$$
(1)

Where G(s) is process, $G_c(s)$ is the multiloop PID controller.

The closed-loop frequency response for each loop can be found by setting $s = j \omega$.

$$H(j\omega,\lambda) = G(j\omega)G_c(j\omega,\lambda)[I + G(j\omega)G_c(j\omega,\lambda)]^{-1}$$
⁽²⁾

It can be expressed in terms of its magnitude and phase,

$$H(j\alpha,\lambda) = |H(j\alpha,\lambda)| \angle H(j\alpha,\lambda)$$
(3)

화학공학의 이론과 응용 제 11 권 제 1 호 2005 년

The magnitude of $H(i\omega, \lambda)$ is

$$|H(j\omega,\lambda)| = \left| \frac{G(j\omega)G_{c}(j\omega,\lambda)}{|I+G(j\omega)G_{c}(j\omega,\lambda)|} \right|$$

$$= \frac{|G(j\omega)G_{c}(j\omega,\lambda)|}{|I+G(j\omega)G_{c}(j\omega,\lambda)|}$$
(4)

The phase of $H(j\omega, \lambda)$ is

$$\angle H (j\omega,\lambda) = \angle G (j\omega) - \angle [1 + G (j\omega)G_e(j\omega,\lambda)]$$
⁽⁵⁾

Most MIMO system can be poor performance when their loop gains become high. In this situation, derived from Eq. (4), $H(j\omega\lambda)$ have to be unity at all frequencies; therefore, the magnitude of $G(j\omega)$ must be infinite, it is not true in practice.

The closed-loop resonant frequency response ω_r can be calculated by Eq. (5).

The Bandwidth BW is the frequency $|H(j\omega, \lambda)|$ dropping to 70.7 percent at its zero-frequency value.

The constrained optimization problem for set of closed-loop time constant λ is described by the function below,

$$\min_{\lambda_{i}} \left[(1 - w) \sum_{i} \sum_{i \neq j} M p_{ij} + w \sum_{i} M p_{ii} \right]$$
Subject to $M p_{ii} \ge M p_{ow}$

$$(6)$$

Where $Mp_{ij} = \max \omega H_{ij}$, the function of λ , Mp_{low} is lower bound of diagonal Mp and it should be selected by a value between 1.1 and 1.4[Harris and Mellichamp, 1985]; w is weighting factor for the diagonal Mp. Here, λ_i is a design variable and determines the speed of response of output for the paired setpoint change. By solving optimization function (6), we can find optimum value of λ_i that minimizes overshoots and disturbance rejection in the loops while all Mp_{ii} must satisfy the constraint. The weighting factor is just given number. Accordingly our studiedness, it is chosen from 0.5 to 0.75 for well-balance in multiloop PID controllers.

1.2. Decentralized PI/PID controller design for MIMO systems

The tuning of decentralized PI/PID controllers for MIMO systems is more complicated problem due to loop interaction and we cannot be directly applied the approaches of SISO system to MIMO system. Recently, several tuning schemes for multiloop PI/PID controllers are proposed base on frequency-domain analysis such as BLT method (Luyben, 1986). Ho et al. (1997) proposed an analytical method for tuning multiloop PID controllers by specifying the gain and phase margins, Lee et al. (1997) proposed a multiloop control system design method in which the proportional gains and integral times are designed sequentially. Here, our proposed method is based on frequency-domain analysis also.

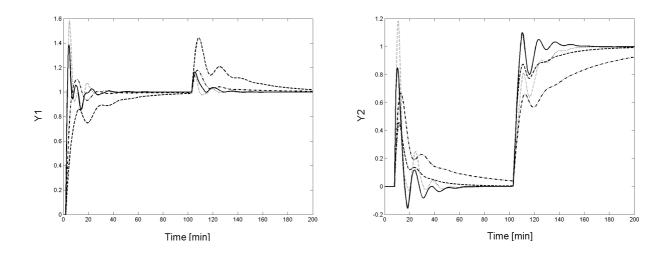


Fig. 1. Set point responses of multiloop PI control systems for Wood and Berry column. (Solid line: proposed, dash dotted line: BLT, dotted line: SAT, dashed line: DLT).

According to Lee at al (1998a), the proportional and derivative gain is given by

$$K_{ci} = f'_i(0)$$
 ; $\tau_{Di} = \frac{f'_i(0)}{2K_{ci}}$ (7)

Analytical tuning rule for integral gain can be obtained by

$$\tau_{Ii} = -\frac{(G'_{ii+}(0) - n_i \lambda_i) K_{ci}}{(G^{-1}(0))_{ii}}$$
(8)

Where G_{ii+} is non –minimum part of G_{ii} and is chosen to be the all pass form, λ_i is an adjustable constant for system performance and stability, n_i is chosen as IMC controller to be realizable, $G_{ii+}(0) = 1$ is necessary for the controlled variable to track its setpoint.

2. Simulation study

Example: Consider an eight trays + reboiler distillation column separating methanol and water (Wood and Berry column model) which was studied by Luyben in 1986.

$$G(s) = \begin{bmatrix} \frac{12.8e^{-s}}{16.7s+1} & \frac{-18.9e^{-3s}}{21s+1} \\ \frac{6.6e^{-7s}}{10.9s+1} & \frac{-19.4e^{-3s}}{14.4s+1} \end{bmatrix}$$
(9)

In case study, the simulation results show that the proposed tuning method for MIMO systems compares favorably with BLT [7], DLT [1] and SAT [6] methods. The optimum closed-loop time constant λ for Wood and Berry column, λ , is found by solving the optimization function which was proposed by the Eq.6, it is in turn as 0.013/4.470 for loop 1 and loop 2. The results tuning are listed in table 1. The Fig.1 shows that the proposed method gives the MIMO control systems with well-balanced and robust responses.

Process		Proposed	SAT	DLT	BLT
WB	λ	0.013	-	6.0	-
		4.470	-	6.0	-
	K _c	1.326	0.868	0.22	0.375
	-	-0.108	-0.087	-0.14	-0.075
	$ au_{I}$	8.557	3.246	17.2	8.29
	1	7.767	10.40	15.9	23.6
	$ au_{\scriptscriptstyle D}$		-	-	
	IAE1*	2.720	4.00	10.94	5.11
		5.560	6.670	5.38	16.8
	IAE2	1.091	0.806	9.66	3.38
		7.621	11.83	10.68	32.7

Table 1. Tuning results by the proposed PI method and various methods for WB column

IAE1*: IAE for unit step change in loop 1.

Conclusions

In this paper, the Mp criterion based analytical design of multiloop PID controllers for desired closed-loop responses was proposed based on the analytical method by Lee et al. (2004) in which the proportional gain and derivative time constant are designed by neglecting of off-diagonal elements while the integral term is designed by taking the off-diagonal element fully into account. The design parameter is the closed-loop time constant between set point and the corresponding outputs. Mp tuning criterion was applied to find optimal design parameter which compromises performance and stability in the multiloop system. The resulting multiloop PID controllers have the closed-loop responses to meet desired performance and robustness as closed as possible.

Acknowledgement

This research was supported by the Program for the Training of Graduate Students in Regional Innovation which was conducted by the Ministry of Commerce, Industry and Energy of the Korea Government.

References

- [1] Jung, J., Choi, J.Y, Lee, J., "One-Parameter Method for a Multiloop Control System Design" *Ind. Eng.Chem.Res.* 1999, 38, 1580-1588
- [2] Lee, Y., Lee, M., Park, S. and Brosilow, C., "PID Controller Tuning for Desired Closed Loop Responses for SI/SO Systems," *AIChE J.*, **44**,106 (1998a).
- [3] Lee, Y., Park, S. and Lee, M., "PID Controller Tuning to Obtain Desired Closed Loop Responses for Cascade Control Systems," *Ind. Eng.Chem. Res.*, **37**, 1859 (1998b).
- [4] Lee, D.Y., Lee, M., Lee, Y., and Park, S., "Mp Criterion Based Multiloop PID Controllers Tuning For Desired Closed-Loop Responses,"*Korean.J. Chem.Eng*, **20**(1), 8-13, (2003).
- [5] Lee, M., Lee, K., Kim, C., and Lee, J., "Analytical Design of Multiloop PID Controllers for Desired Closed-Loop Responses,"*AIChE J.*, 50, 1631-1635, (2004).
- [6] Loh, A.P., Hang C.C., Quek, C.K., Vasnani, V.N., "Autotuning of Multivariable Proportional-Integral Controllers Using Relay Feedback". *Ind. Eng. Chem. Res.* 1993, **32**, 1002-1007.
- [7] Luyben, W. L., "Simple Method for Tuning SISO Controllers in Multivariable Systems," *Ind. Eng. Chem. Process Des. Dev.*, **25**, 654(1986).

화학공학의 이론과 응용 제 11 권 제 1 호 2005 년