## Pyrolysis of Biomass using Nickel Catalysts of Various Compositions for H<sub>2</sub> production

## <u>최용근</u>, 제이타, 이준철, 김재형, 박홍선, 손재익, 박대원\* 서울산업대학교 에너지환경대학원 (daewon@snut.co.kr\*)

Catalytic pyrolysis of biomass using Ni/Al<sub>2</sub>O<sub>3</sub>, Ni/CeO<sub>2</sub> and Ni/Al<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> catalysts of various compositions prepared by coprecipitation method has been studied to produce H<sub>2</sub>-rich product gases. In Ni/Al<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> catalysts, Ni was maintained at the composition of 30wt%, whereas alumina and ceria are changed to 40wt%:60wt%, 50wt%:50wt% and 60wt%:40wt%. The papers used in daily writing purposes were adapted as biomass sample. The furnace temperature was increased to 800°C with heating rate of 10°C/min. and was maintained the temperature at 800°C for various residence time. 30wt%/(50wt%-50wt%) Ni/Al<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> sample had shown the best performance in pyrolysis process. In each catalyst, residence time at final temperature has shown their performances to the best. The volume of H<sub>2</sub>-gas has reached its highest value (5.22 ml) in the case of Ni/Al<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> 30wt%/(50wt%-50wt%) catalyst. It is concluded that Ni/CeO<sub>2</sub> catalysts are better in their performances than those of Ni/Al<sub>2</sub>O<sub>3</sub> catalysts; whereas in Ni/Al<sub>2</sub>O<sub>3</sub>-CeO<sub>2</sub> catalysts, catalytic activity changes with change in the composition of alumina and ceria. Similarly, residence time at final temperature dis composition of alumina the pyrolysis process.