

Chapter 1&2. 가

- 가 7가 chemical blocks –

- (1) Ethylene
- (2) Propylene
- (3) Butenes & Butadiene
- (4) Methane
- (5) Benzene
- (6) Toluene
- (7) Xylene

- 가 : olefins

- (1) Ethylene
 - (2) Propylene
 - (3) Butenes & Butadiene
- (olefins)

- – (BTX)

- (5) Benzene
 - (6) Toluene
 - (7) Xylene
- (Aromatic hydrocarbon)

- 가

- (4) Methane

- (petrochemical) – petroleum natural gas

- 7가 chemical blocks

–synthesis gas (syngas) : mixture of carbon monoxide(CO) and

hydrogen(H₂)

- Natural gas (가)

- methane

, CO₂, H₂S

└ Associated gas – gas ↗ crude oil

— Non-associated gas – gas ↗ crude oil

- source of energy.

- Dry natural gas –

가

85~95% ↗ methane.

- Wet natural gas –

↗ 0.3 gal/1000ft³

Condensable hydrocarbon

- Dry gas water content (humidity)

treatment ↗

- Dry sour gas (or sour natural gas) hydrogen sulfide (H₂S) CO₂

. natural gas acid gases hydrogen sulfide

CO₂

- Acid gas removal – mono and diethanolamines (MEA, DEA)

molecular sieve (zeolite)

- Natural gas humidity adjustment – hydrate (powder)

H₂O

- Hydrocarbon + H₂O → hydrate formation (under pressure and temp in gas pipe line).

- Glycol H₂O

() ethylene glycol, diethylene glycol .

- , water is soluble in EG, but gas is not soluble.

- Silica gel molecular sieve H_2O

• Wet natural gas condensation hydrocarbon

- 가 (liquid propane)

• Condensable hydrocarbon (natural gas liquids)

- propane liquefied
petroleum gas(LPG) 가 . LPG propane butane

• Natural gas

(1) Humidity

(2) Condensable hydrocarbon

(3) Hydrogen sulfide, CO_2 methane

• Liquefied Natural gas :

가 가 ()

water vapor < 10 ppm

carbon dioxide < 100 ppm

$\text{H}_2\text{S} < 50 \text{ ppm}$

• Associated gas ()

- oil 가 가 , associated gas
excess gas .

• Natural gas liquids (NGL) – natural gas associated gas

.(ethane~pentane).

- LPG propane butane .
- Petroleum composition and classification.
- Petroleum (crude oil)
 - natural gas, gasoline, naphtha, kerosene, fuel and lubricating oils, paraffin wax, etc.
 - nonhomogeneous mixture . , main hydrocarbon .(S, O₂, N₂, CH compounds) , dissolved gases, metallic compound.
 - Specific crude oil , refinery process . high cyclo paraffin (naphthene) crude oil ethylene aromatics .
- (petroleum) hydrocarbon :
 - (1) hydrocarbon
 - (2) gasoline fraction normal paraffins (straight chain)
 - branched paraffins
 - alkyl cyclopentanes
 - alkyl cyclohexanes
 - alkyl benzenes
 - (3) 5 gasoline fraction .(see page9)
- Nonhydrocarbon compounds :
 - Sour crude oil > {(0.05cubic feet of H₂O)/(100 gallons)}
 - Crude oil density γ sulfur (S)

- Hydrocarbon H₂S, nitrogen, oxygen compounds, metallic compounds .
 - (crude oil) classification
 - (1) Light Paraffinic – wax (hydrocarbon)
 - (2) Paraffinic – wax asphalt
 - (3) Naphthenic or asphaltic – wax asphalt
 - (4) Aromatic
 - aromatic
 - Mixed crude oil paraffinic naphthenic
 - The correlation Index, BMCI (paraffinic?, mixed? or aromatic?) BMCI(the us Bureau of Mines Correlation Index)

BMCI=48,640/K + 473.7/d – 456.8 (0 for paraffins, 100 for benzene).

K= the mid-boiling point of a fraction in Kelvin degrees.

D= the specific gravity of the fraction at 60/60 °F
 - Crude oil quality –
 - (1) specific gravity – density .
 - API (degrees) = $(141.5) / (\text{Sp. Gr. } 60/60 \text{ } ^\circ\text{F}) - 131.5$
 - (2) Pour point – oil γ† wax†crude oil
?
 - (3) Sulfur – further treatment is needed. (corrosive and reduce the lifetime of the engine).
 - (4) Carbon residue – heating coke . Do not evaporate.

(5) Ash content – amount of ash left after burning oil.

- metallic salts, metal oxide, silicon oxide
- Total World Oil Reserves – Jan.1, 1978
 - 646 billion barrels
 - 1 barrel = 31.5 gallon = 120 l
- 2.2

1. 가 (65-90%) ,	20 °C	가 .
2. (C_5, C_6)) ($C_7 \sim C_9$)	70~140 °C 140~200 °C	. 가 . 가 ,
3. gas oil	175~275 °C 200~370 °C	$C_9 \sim C_{16}$, , , $C_{15} \sim C_{25}$.
4. (residual oil)	370 °C	.

“ ”		,
		(see 2.2 also)

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Refinery Processes

()

. Crude oil

Fuel(64%) + Petrochemical (6%)

-1979

Fuel (89%) + Petrochemical (11%)

-1990

. Crude oil

two commercial processes

Heavy Oil Cracking (HOC)

Thermal pyrolysis of the resulting hydrocarbon

. Major Products

Olefins-ethylene, propylene, and mixed C4's

Aromatic hydrocarbon (BTX)

. Refinery Processes

(1) Physical separation processes-

Distillation

Absorption

Adsorption

Extraction

Distillation – a physical separation

Process based on differences in boiling points ().

- processing . gasoline, naphtha,
gas oil, diesel oil . vacuum distillation
- .
- Vacuum distillation: to avoid cracking the long-chain hydrocarbons.
 - [] Gas oil – top product
 - [] Lube oil
 - [] Asphalt – bottom
- Vacuum distillation middle distillates 가 .

Absorption – a process used to collect gases in a liquid absorbent.

Adsorption – a process used to free petroleum gases from trace amounts of undesired gases or vapors by adsorbing them on a solid material.
. Solid material – have a large surface area. (molecular sieve, silica gel, alumina)

Solvent extraction – Liquid solvents

() Propane deasphalting – the liquid propane dissolves paraffinic hydrocarbons and leaves aromatic and asphaltic material.

(2) Conversion Processes – to produce more gasoline and better gasoline.

. The four major gasoline making and octane boosting processes are:

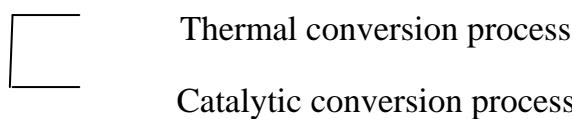
catalytic cracking()

catalytic reforming ()

hydrocracking (γ†)

alkylation ()

Petroleum Refinery Processes (Conversion)



(1) Thermal conversion process – the first process used to increase gasoline production.

viscosity breaking (visbreaking)

– improvement of its pour point by including a mild thermal-cracking step.

coking – a severe thermal cracking process used to obtain light

products and coke from topped crude and heavy residues which cannot be directly fed into a catalytic cracking unit because of their high metal and asphaltic content.

Steam cracking

– steam thermal cracking olefin

(2) Catalytic conversion process

catalytic reforming process () catalytic cracking
process ()
hydrocracking () hydrotreating ()
hydrorefining ()
,

alkylation	dimerization
polymerization	isomerization

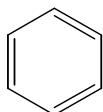
catalytic process .

Catalytic reforming process () –

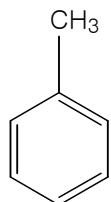
A process used to produce a higher quality gasoline. The feed to a catalytic reforming unit is naphtha, either virgin or produced from a thermal or catalytic hydrocracking unit.

- Benzene, toluene and xylene (BTX) are produced from naphtha during catalytic reforming by two distinct types of reaction.
 - () The dehydrogenation of naphthenes :

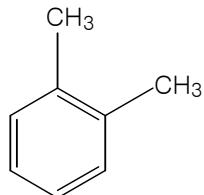
- cyclohexene -> benzene



C₇ naphthene -> toluene

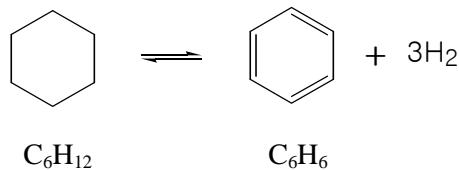


C₈ naphthene -> xylene



o -xylene/ m -xylene/ p -xylene

- . Catalyst – the catalysts generally used for catalytic reforming.
platinum .
- . Reforming reaction – occur at different rate and degrees of conversion depending on the themperature, hydrogen partial pressure and catalyst used.
- () Aromatization – the dehydrogenation of cyclohexanes to benzene and methyl benzenes is completely fast and endothermic.
(ΔH = 49.08 kcal/mol)

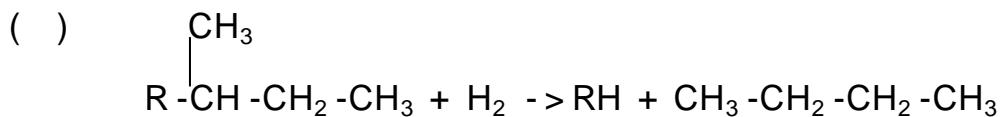


- The production of benzene is favored by high temp. and low pressure.

Hydrocracking – is a cracking reaction where by high molecular weight hydrocarbons pyrolyze to lower molecular weight paraffins and Olefins in the prsence of hydrogen.

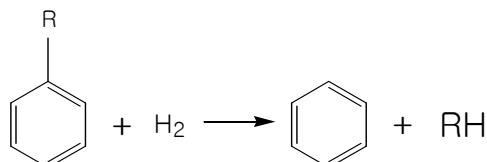
- . Hydrocracking is a hydrogen-consuming reaction that leads to higher gas

production.



Dealkylation – like hydrocracking, is a hydrogen-consuming reaction, At higher hydrogen partial pressure, dealkylation is more favorable.

()



- 가 , yield .

- Hydrocracking – the most versatile modern petroleum refining processes.
is specially adapted to the processing of low value stocks such as those
that are not suitable for a catalytic cracking or reforming unit because of
high metal, nitrogen and/or sulfur content.
- Is also suitable for high aromatic feeds which cannot be processed easily
by conventional catalytic cracking processes.

catalytic cracking – the main advantage is increased gasoline production,
and the formation of hydrocarbon components having high antiknock
properties. Another advantage is the production of C₃ and C₄
hydrocarbons for LCP uses.

Hydrogen reforming (or hydrogen treating)-

a process designed to reduce the sulfur content of atmospheric residue,
vacuum gas oil, and vacuum residues.

Isomerization] do not increase the quantity of gasoline but do contribute
Alkilation to the quality of the gasoline.
Dimerization

- Isomerization – a small volume but important refinery process. Normal butane is isomerized to isobutene to be used for the alkylation of isobutylene and other olefins for the production of high octane hydrocarbons such as isooctane.
- Alkylation – generally applies to the acid catalyzed reaction between isobutene and various light olefins. The product is highly branched paraffin hydrocarbons, alkylate, used for blending to improve the octane number of gasoline.
- Dimerization – propylene- propane mixture to give isohexanes or propylene-butene mixture to yield isoheptenes: to upgrade the octane number. Both phosphoric acid and sulfuric acid are used as catalysts.
- Octane value – a number indicating the degree of knocking of a fuel mixture under standard test conditions.
 - Pure normal heptane(a very high knocking fuel)is arbitrarily assigned an octane number of zero, while isooctane (a branched chain paraffin) is assigned 100. Thus a rating of 80 for a given fuel indicates that its degree of knocking in a standard test engine is equal to that of a mixture of 80 parts isooctane and 20 parts n-heptane (80).
 - Lead alkyl compound (usually tetraethyl or tetramethyl lead) octane value $\nabla 100$ unleaded

(Petroleum Refining Reactions)

styrene ,
propylene .

(h) (dimerization)

- 가
n-butane isobutene , n-pentane
isopentane, n-hexane -> isohexane , n-
butene -> isobutene . o-, m-xylene -> p-xylene

(i) 가 (hydrocracking)

- , , H₂S, NH₃, H₂O 가