Chapter 2. 가

•	가	7가	chemical blocks -	
(1) Ethylone				

- (1)Ethylene
- (2)Propylene
- (3) Butenes & Butadiene
- (4) Methane
- (5)Benzene
- (6) Toluene
- (7) Xylene

- (1)Ethylene
- (2)Propylene —
- (3)Butenes & Butadiene (olefins)

- (5) Benzene
- (6) Toluene —
- (7) Xylene (Aromatic hydrocarbon)

```
• 가
(4)Methane
```

• (petrochemical) – petroleum natural gas

• 7가 chemical blocks

synthesis gas (syngas) : mixture of carbon monoxide(CO) and $hydrogen(H_2)$

- Natural gas (가)
 - methane

- Associated gas - gas가 crude oil - Non -associated gas - gas가 crude oil

- source of energy.
- Dry natural gas 가 85~95%가 methane.
- Wet natural gas 7 0.3 gal/1000ft³

	. Condensa	ble hydrocarbon	
• Dry gas v	vater content (humid	lity)	
	treatment가		
• Dry sour gas	(or sour natural gas)	hydrogen sulf	ide (H ₂ S)
	CO ₂	. natural gas	acid gases
	hydrogen sulfid	e CO ₂ .	
Acid gas remov	al – mono and diethan	olamines (MEA, D	DEA)
	. molecular	sieve (zeolite)	
Natural gas h	umidity adjustment –	hydrate (powder	
)	H_2	0
• Hydrocarbon +	$H_2O \longrightarrow hydrate for$	rmation (under pi	essure and
	temp in gas pipe line	a).	
• Glycol H₂O	_		

, water is soluble in EG, but gas is not soluble.

 H_2O

molecular sieve

() ethylene glycol, diethylene glycol .

- Silica gel

```
• Wet natural gas condensation hydrocarbon
             가
                     (liquid propane
• Condensable hydrocarbon (natural gas liquids)
         propane
            liquefied petroleum gas(LPG)가 . LPG
                        butane
            propane
· Natural gas
   (1) Humidity
   (2) Condensable hydrocarbon
   (3) Hydrogen sulfide, CO<sub>2</sub>
                                    methane
· Liquefied Natural gas:
    가 가
        water vapor < 10 ppm
        carbon dioxide < 100 ppm
        H_2S < 50 \text{ ppm}

    Associated gas (

                                 가 가
                oil
                                                     , associated
```

gas excess gas .

- Natural gas liquids (NGL) natural gas associated gas
 .(ethane~pentane).
- LPG propane butane .
- · Petroleum composition and classification.
- Petroleum (crude oil)
 - natural gas, gasoline, naphtha, kerosene, fuel and lubricating oils, paraffin wax, etc.
 - nonhomogeneous mixture . , main hydrocarbon
 .(S, O_2 , N_2 , CH compounds) , dissolved gases, metallic compound.
 - Specific crude oil ,
 refinery process . high cyclo
 paraffin (naphthene) crude oil ethylene
 aromatics .
- (petroleum) hydrocarbon :
 - (1) hydrocarbon
 - (2) gasoline fraction normal paraffins (straight chain) branched paraffins

		alkyl cy	clopentar	nes	
		alkyl cy	clohexan	es	
		alkyl be	nzenes		
(3)	5	gasoline fr	action		
	.(see page9))			
Nonhy	drocarbon co	ompounds:			
-	Sour crude	oil > {(0.050	cubic fee	t of H ₂ O)/(100 g	allons)}
-	Crude oil	density가		sulfur (S)	
-	Hydrocarbo	on		H2S,nitrogen,	oxyger
	compounds	, metallic com	pounds		
(c	rude oil) c	lassification			
(1) Li	ight Paraffin	ic –	wax	(hydrocarbon)
(2)Pa	araffinic –	wax	asphal	t .	
(3)N	aphthenic or	asphaltic –	wax	asphalt	
(4)A	romatic				
	– arc	matic			

• The correlation Index, BMCI

Mixed crude oil paraffinic

naphthenic

(paraffinic?, mixed? or aromatic?)

BMCI(the us Bureau of Mines Correlation Index)

BMCI=48,640/K + 473.7/d - 456.8 (0 for paraffins, 100 for benzene).

K = the mid -boiling point of a fraction in Kelvin degrees.

D= the specific gravity of the fraction at 60/60 F

- Crude oil quality
 - (1) specific gravity density .

API (degrees) =
$$(141.5)$$
 / (Sp. Gr. $60/60$ F) $- 131.5$

(2)Pour point - oil 가 wax가 crude oil

?

- (3)Sulfur further treatment is needed. (corrosive and reduce the lifetime of the engine).
- (4) Carbon residue heating coke . Do not evaporate.
- (5) Ash content amount of ash left after burning oil.
 - metallic salts, metal oxide, silicon oxide
- Total World Oil Reserves Jan.1, 1978

646 billion barrels

1 barrel = 31.5 gallon = 120 l

• 2.2

1. 가	20 °C	가 .
(65 -90%)		
, ,		
2. (70~140 ℃	
)		. 가
(C ₅ ,C ₆)		. 가
		,
		가
	4.40 000 00	
	140~200 ℃	
(C ₇ ~C ₉)		
3. gas oil		
		$C_9 \sim C_{16}$, ,
	175~275 ℃	,
		C ₁₅ ~C ₂₅
	000 070 %	015 025
	200~370 ℃	
		•
4.		
	370 ℃	
(residual oil)		

	,
٠٠ ,,	

(see 2.2 also)

```
p. 60
```

Refinery Processes

()

. Crude oil

-1979

Fuel (89%) + Petrochemical (11%)

-1990

. Crude oil

two commercial processes

Heavy Oil Cracking (HOC)

Thermal pyrolysis of the resulting hydrocarbon

. Major Products

Olefins-ethylene, propylene, and mixed C4's

Aromatic hydrocarbon (BTX)

- . Refinery Processes
 - (1) Physical separation processes-

Distillation

Absorption

Adsorption

Extraction

Dis	stillation – a physical se	eparation	
	Process based on diffe	erences in boiling points (
).		
-		processing .	gasoline, naphtha,
	gas oil, diesel oil		vacuum distillation
-	Vacuum distillation: to	avoid cracking the long-cl	hain hydrocarbons.
	Gas oil – top pro	oduct	
	Lube oil		
	Asphalt – botto	om	
-	Vacuum distillation	middle distillates	가 .
	Absorption – a process	s used to collect gases in a	liquid absorbent.
	Adsorption – a proces	s used to free petroleum g	gases from trace amounts
	of undesired gases or	vapors by adsorbing them	on a solid material.
	. Solid material – have	e a large surface area. (m	olecular sieve, silica gel,
alumin	na)		
	Solvent extraction – 1	Liquid solvents	

() Propane deasphalting - the liquid propane dissolves paraffinic
hydrocarbons and leaves aromatic and asphaltic material.
(2) Conversion Processes – to produce more gasoline and better gasoline.
. The four major gasoline making and octane boosting processes are:
catalytic cracking()
catalytic reforming ()
hydrocracking (가)
alkylation ()
Petroleum Refinery Processes (Conversion)
Thermal conversion process
Catalytic conversion process
(1) Thermal conversion process – the first process used to increase gasoline
production.
viscosity breaking (visbreaking)
- improvement of its pour point by including a mild thermal-cracking
step.
coking - a severe thermal cracking process used to obtain light
products and coke from topped crude and heavy residues which cannot
be directly fed into a catalytic cracking unit because of their high metal

and asphaltic conten	ıt.		
Steam cracking			
– steam	thermal cracking	olefin	
(2) Catalytic conversion pr	ocess		
catalytic reform	ing process () catalytic cr	acking
process ()			
hydrocracking (가)	hydrotreating (
가)			
hydrorefining (가)		
,			
alkylation		dimerization	
polymerization		isomerization	
catalyt	tic process .		
Catalytic reforming pro	ocess () –	
A process used to prod	luce a higher quality	gasoline. The feed to a ca	atalytic
reforming unit is nap	htha, either virgin	or produced from a them	mal or
catalytic hydrocracking	g unit.		
- Benzene, toluene and	d xylene (BTX) are	produced from naphtha	during
catalytic reforming by	y two distinct types o	of reaction.	
- () The dehydrogena	ation of naphthenes:		
- cyclohexene -> benze	ene		



C₇ naphthene -> toluene

C₈ naphthene -> xylene

o-xylene/ m-xylene/ p-

xylene

- . Catalyst the catalysts generally used for catalytic reforming. platinum $\,$.
- . Reforming reaction occur at different rate and degrees of conversion depending on the themperature, hydrogen partial pressure and catalyst used.
- () Aromatization the dehydrogenation of cyclohexanes to benzene and methyl benzenes is completely fast and endothermic.

 $(\Delta H = 49.08 \text{ kcal/mol }) \text{p. } 60$

Refinery Processes

()

•	Crude	01

Fuel(64%) + Petrochemical (6%)

-1979

Fuel (89%) + Petrochemical (11%)

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two commercial processes

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Distillation – a physical separation

Process based on differences in boiling points (

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-		processing .	gasoline, naphtha,
	gas oil, diesel oil		vacuum distillation
-	Vacuum distillation: to	o avoid cracking the long-ch	ain hydrocarbons.
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	. Solid material – hav	ve a large surface area. (mo	lecular sieve, silica gel,
alumir	na)		
	Solvent extraction -	Liquid solvents	
	•		
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asphaltic content.
Steam cracking
steam thermal cracking olefin
•

(2) Cat	alytic conversion pro	cess				
	catalytic reforming	process	()	catalytic cracking pr	oces
()					
	hydrocracking (가)		hydrotreating (フ
)						
	hydrorefining (가)			
	,					
	alkylation				dimerization	
	polymerization				isomerization	
	catalytic	e process	s .			

Catalytic reforming process () –

A process used to produce a higher quality gasoline. The feed to a catalytic reforming unit is naphtha, either virgin or produced from a thermal or catalytic hydrocracking unit.

- Benzene, toluene and xylene (BTX) are produced from naphtha during catalytic reforming by two distinct types of reaction.
- () The dehydrogenation of naphthenes :
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$$C_6H_{12} \qquad C_6H_6$$

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hydrocarbons pyrolyze to lower molecular weight paraffins and Olefins in the prsence of hydrogen.

. Hydrocracking is a hydrogen-consuming reaction that leads to higher gas production.

()
$$\mid$$
 CH₃
 R-CH-CH₂-CH₃ + H₂ -> RH + CH₃-CH₂-CH₂-CH₃

Dealkylation – like hydrocracking, is a hydrogen-consuming reaction, At higher hydrogen partial pressure, dealkylation is more favorable.

 $\begin{array}{c} R \\ \downarrow \\ + H_2 \longrightarrow \begin{array}{c} \\ \end{array} + RH \end{array}$

- 가 , yield .

p. 60

Refinery Processes

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Gas oil – top product
Lube oil
Asphalt – bottom
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p. 60

Refinery Processes

()

. Crude oil

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).		
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steam thermal cracking olefin
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(6) Catalytic conversion process
catalytic reforming process () catalytic cracking process
()
hydrocracking (가) hydrotreating (가
)
hydrorefining (フト)
,
alkylation dimerization
polymerization isomerization

catalytic process

Catalytic reforming process () –

A process used to produce a higher quality gasoline. The feed to a catalytic reforming unit is naphtha, either virgin or produced from a thermal or catalytic hydrocracking unit.

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platinum

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()
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 $R - CH - CH_2 - CH_3 + H_2 -> RH + CH_3 - CH_2 - CH_2 - CH_3$

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()

$$+ H_2 \longrightarrow + RH$$

- 가 , yield

p. 60

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(7) Phys	sical separation pr	ocesses-		
Dis	stillation			
Ab	sorption			
Ad	sorption			
Ex	traction			
Distillati	on – a physical se	eparation		
Proc	ess based on diff	ferences in boiling po	ints (
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-		processing	. gasoline, naphtha	ì,
gas	oil, diesel oil		vacuum distillation	
	·			
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	– improvement of its pour point by including a mild thermal-cracking				
step.					
	coking – a severe th	ermal crack	ing process	used to obtain lig	tht products
	and coke from top	ped crude	and heavy	residues which	cannot be
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	asphaltic content.				
	Steam cracking				
	– steam	thermal cra	cking	olefin	
(8) Ca	ntalytic conversion pr	ocess			
	catalytic reforming	g process ()	catalytic crack	ing process
()				
	hydrocracking (가)	hydrotreating	;(가
)					
	hydrorefining (가))		
	,				
	alkylation			dimerization	
	polymerization			isomerizatio	n
catalytic process .					
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()

$$+ H_2 \longrightarrow + RH$$

- 가 , yield

- Hydrocracking the most versatile modern petroleum refining processes.
 - is specially adapted to the processing of low value stocks such as those that are not suitable for a catalytic cracking or reforming unit because of high metal, nitrogen and/or sulfur content.
 - Is also suitable for high aromatic feeds which cannot be processed easily by conventional catalytic cracking processes.
- (d) catalytic cracking the main advantage is increased gasoline production, and the formation of hydrocarbon components having high antiknock properties. Another advantage is the production of C_3 and C_4 hydrocarbons for LCP uses.
- (e) hydrogen reforming (or hydrogen treating) a process designed to reduce the sulfur content of atmospheric
 residue, vacuum gas oil, and vacuum resides.
- (f) Isomerization do not increase the quantity of gasoline but do.Alkilation contribute to the quality of the gasolineDimerization
- Isomerization a small volume but important refinery process.
 Normal butane is isomerized to isobutene to be used for the

alkylation of isobutylene and other olefins for the production of high octane hydrocarbons such as isooctane.

- Alkylation generally applies to the acid catalyzed reaction between isobutene and various light olefins. The product is highly branched paraffin hydrocarbons, alkylate, used of blending to improve the octane number of gasoline.
- Dimerization propylene propane mixture to give isohexanes or propylene - butene mixture to yield isoheptenes: to upgrade the octane number. Both phosphoric acid and sulfuric acid are used as catalysts.

Octane value

- a number indicating the degree of knocking of a fuel mixture under standard test conditions.
- Pure normal ehptane(a very high knocking fuel)is arbitrarily assigned an octane number of zero, while isooctane (a branched chain paraffin) is assigned 100. Thus a rating of 80 for a given fuel indicates that its degree of knocking in a standard test engine is equal to that of a mixture of 80 parts isooctane and 20 parts n-heptane (80).
- lead alkyl compound (usually tetraethyl or tetramethyl

```
unleaded
       (Petroleum Refining Reactions).
                               가
                    (steam cracking) - n - ,
   (a)
                             가
                  (catalytic cracking) -
   (b)
       가
                                 5~12
              가
                      (hydrocracking) -
   (c)
                               H<sub>2</sub>S, NH<sub>3</sub>, H<sub>2</sub>O
   (d)
            (polymerization, oligomerization)
                        H_2SO_4
                                      H_3PO_4
              가
                                                       가
             (oligomers)가
              (alkylation)
    (e)
```

read) octane value가 100

```
(
        ) 가
                                        가
                  가
            (catalytic reforming)
(f)
                                            BTX
                  가
         (dehydrogenation)
(g)
                          styrene
                             propylene
        (dimerization)
(h)
                    가
               n -butane isopentane, isobutane
   , n -butane isopentane,
n -hexane ____ isohexane, , n -butane ____
isobutene
                                  , o-,m-xylene
→ p-xylene
         가 (hydrotreating) –
(i)
                                      H_2S, NH_3,
H_2O
      가
```