# Chapter 9 Generation of (Nano)Particles by Growth

#### 9.1 Nucleation

## (1) Supersaturation

Thermodynamics assumes a phase change takes place when there reaches

Saturation of vapor in a gas,

Saturation of solute in a solvent or

Saturation of solute in a solid solution....

\* Vapor pressure and solubilities indicate the saturation...

In real world, the phase change requires a certain degree of supersaturation, accompanying a formation of nuclei in the media...

Supersaturation of growth species, S

$$S = \frac{p}{p_0} > 1$$

$$S = \frac{c}{c_0} > 1$$

where p: partial pressure of the species i in the gas phase  $>p_v$ 

c: concentration of species i in the solution

 $p_0$ ,  $c_0$ : vapor pressure and saturation concentration of the species i

## (2) Formation of Nuclei (Nucleation)

### 1) Critical Nuclei and Energy Barrier

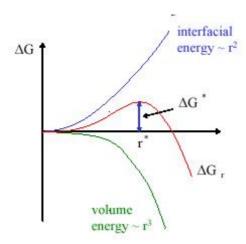
Gibbs free energy change for a sphere of the growth species from molecules

$$\Delta G = \pi x^2 \sigma + \frac{\pi x^3}{6} \Delta G_v$$

interfacial volume

energy energy

where 
$$\Delta G_v = -\frac{kT}{v_m} lnS$$



Newly formed nucleus is stable only when its radius exceeds a critical size r\*(or x\*)...

At critical size  $r^*(x^*)$ 

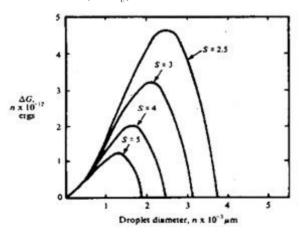
$$\left. \frac{d\Delta G_v}{dx} \right|_{x = x^*} = 0$$

By some manipulation

$$x^* = -\frac{4\sigma}{\Delta G_v} = -\frac{4\sigma v_m}{kT \ln S}$$
 (\*) Diameter of critical nucleus

$$\Delta G^* = \frac{16\pi\sigma}{(3\Delta G_v)^2}$$

Energy barrier against nucleation



 $\Delta G_v$  for formation of water droplet

\* From (\*)

$$\ln S = \ln \left( \frac{p_x}{p_0} \right) = \frac{4\sigma v_m}{k T x}$$

Kelvin equation

- Vapor pressure elevation (or boiling point lowering) of small particles
- 2) Nucleation rate [number of nuclei formed /(timevolume of medium)] Homogeneous nucleation
- For vapor-to-droplet in gas

$$R_N = \frac{p^2}{(2\pi m)^{1/2} (kT)^{3/2}} (\pi x^2) \exp\left(-\frac{\Delta G^*}{kT}\right)$$

where m: molecular mass

- For solute-to-particles in solution

$$R_N = \frac{C_0 k T}{3\pi x_m^3 \mu} exp\left(-\frac{\Delta G^*}{k T}\right)$$

where  $C_0$ : initial concentration  $x_m$ : molecular diameter

\* Critical saturation ratio, S at  $R_N = 1.0$ For water vapor at  $300^{\circ}$ C,  $S_{crit} = 3.1$ 

## Heterogeneous nucleation

- Formation of nuclei on existing foreign surface

$$\varDelta \, {G^*}_{het} = \varDelta \, {G^*} \frac{(2 + \cos \theta)(1 - \cos \theta)^2}{4}$$

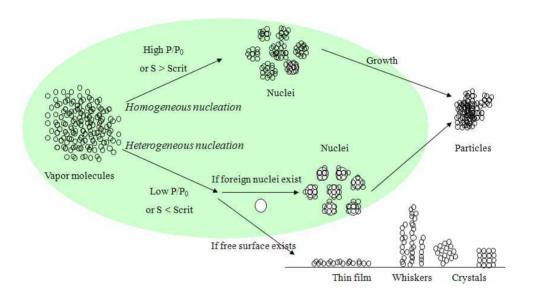
where  $\theta$ : angle of contact

Since  $\Delta G^*_{het} \leq \Delta G^*$ ,

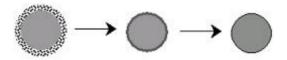
- Heterogeneous nucleation is easier than homogeneous nucleation in most cases...
- \* Criteria for homo or heterogeneous nucleation For  $S > S_{crit}$ , homogeneous nucleation For  $S < S_{crit}$ , heterogeneous nucleation
- \* If foreign surface is supplied by foreign nuclei(ions, clusters...), particle growth on the existing nuclei after homogeneous nucleation. This resulted in the growth of monodisperse particles...

ex. artificial rain formation

\* If the foreign surface is supplied by the plain surface, thin film or whiskers will grow...



# 9.2 Growth by Condensation



 Condenstaion: growth of particles by collision of individual molecules followed by sticking...

### (1) Growth Law

- In general condensation occurs in diffusion limited condition...

In free molecule regime

$$\frac{dx}{dt} = \frac{2v_m}{(2\pi mk \, T)^{1/2}} (p - p_x)$$

In continuum regime

$$\frac{dx}{dt} = \frac{4Dv_m}{kTx}(p - p_x)$$

In terms of particle volume, v

$$\frac{dv}{dt} = \frac{d\left(\frac{\pi x^3}{6}\right)}{dt} = \frac{\pi}{6} 3x^2 \frac{dx}{dt} = \frac{\pi}{2} x^2 \frac{4Dv_m}{kTx} (p-p_x) = \frac{2\pi Dv_m x}{kT} (p-p_x)$$

- If  $p < p_x$ , evaporation occurs..
- For growth from liquid phase

$$\frac{dx}{dt} = \frac{4Dv_m}{r}(c - c_x)$$

- \*  $\frac{dx}{dt}$  is called "growth law".
- \* Variation in size decreases as growth by condensation proceeds!

## (2) Ostwald ripening

From Kelvin equation

$$\ln S = \ln \left( \frac{p_x}{p_0} \right) = \frac{4\sigma v_m}{k Tx}$$

For the two particles,  $x_1 \gg x_2 \ \rightarrow \ c_{x_1} << c_{x_2}$ 

Solute will deposit onto the surface of the larger particle, whereas the small particle has to continue dissolving...

#### Example.

A 30- $\mu$ m-diameter water droplet is evaporating in a chamber. The chamber temperature is  $20^{\circ}$ C, and the pressure is 760mmHg. The chamber relative humidity is 50%. Find the droplet evaporation rate in grams of water lost per second. Diffusion coefficient of water vapor in air is  $0.251 \text{cm}^2/\text{s}$  and vapor pressure at  $20^{\circ}$ C is 17.50 mmHg.

$$k := 1.38 \cdot 10^{-16} \frac{\text{erg}}{\text{K}}$$

$$p := \frac{17.5}{760} \text{ atm} \qquad p := px \cdot 0.5$$

$$x := 30 \times 10^{-6} \text{m}$$

$$vm := \frac{18 \text{gm}}{6.023 \cdot 10^{23}} \qquad D := 0.251 \frac{\text{cm}^2}{\text{s}}$$

$$T_{\text{AC}} := 293 \text{K}$$

$$+$$

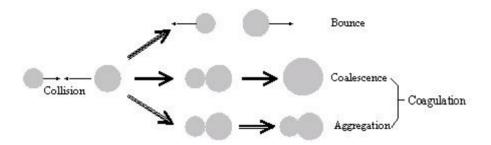
$$I := \frac{2\pi D \cdot vm \cdot x}{k \cdot T} (p - px)$$

$$I = -4.079 \times 10^{-11} \frac{\text{kg}}{\text{s}}$$

# 9.3 Growth by Coagulation

#### (1) Introduction

- Growth as a result of collision of a particle with other particle and subsequent sticking with each other...



- Sources of collision

Brownian motion

External force fields

Particle-particle interaction (polar, coulombic)

- Coalescence

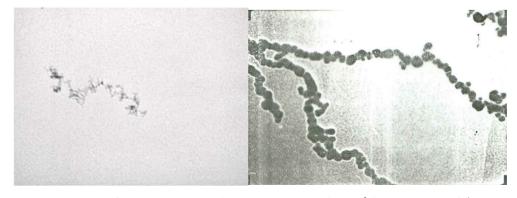
Spherical growth: liquid-phase growth

Occurs for most liquid particles and for rapid sintering solid particles



- Aggregation(Agglomeration)

Nonspherical growth keeping identities of primary particles Solid-phase growth



Aggregation of TiO<sub>2</sub> nanoparticles

Aggregation of iron nanoparticles

### (2) Mathematical Description for Coagulation

Let

 $N_{i,j}$ : Number of collisions occurring per unit time per unit volume of medium between the particles having diameters (volumes)  $d_i(v_i)$  and  $d_j(v_j)$  respectively.

$$N_{i,j} = b_{i,j} n_i n_j$$

$$where$$

 $n_i$ ,  $n_j$ : number concentration of colliding particles  $v_i$ ,  $v_j$ , respectively  $(no./cm^3)$ 

i, j: number of basic units making particles (e.g. i-mer and j-mer)

In terms of continuous size distribution

$$N(v_i,v_j) = b(v_i,v_j)n(v_i)n(v_j)dv_idv_j$$
 where  $b_{i,j} = b(v_i,v_j)$ : collision frequency function "Coagulation coefficient"

- Coagulation resulted in the increase in size but decrease in the number concentration of particles...

In discrete notation

$$\frac{d\,n_k}{dt} = \frac{1}{2} \sum_{i\,+\,j\,=\,k}^{N_{i,j}} - \sum_{i\,=\,1}^{\infty} N_{i,k} = \frac{1}{2} \sum_{i\,+\,j\,=\,k}^{N_{i,j}} b_{i,j} n_i n_j - n_k \sum_{i\,=\,1}^{\infty} b_{i,k} n_i$$

In continuous notation

$$\frac{dn(v)}{dt} = \frac{1}{2} \int_{0}^{v} b(v', v - v') n(v') n(v - v') dv' - n(v) \int_{0}^{\infty} b(v, v') n(v') dv'$$

#### (3) Brownian coagulation

For continuum regime

$$\begin{split} b_{i,j} &= \left(\frac{2kT}{3\mu}\right) \!\! \left(\frac{1}{v_i} \!+ \frac{1}{v_j}\right) \!\! \left(v_i^{1/3} \!+ v_j^{1/3}\right) \\ &= \left(\frac{2kT}{3\mu}\right) \!\! \left(\frac{1}{x_i} \!+ \frac{1}{x_j}\right) \!\! \left(x_i \!+ v_j\right) \end{split}$$

For polydisperse particles

When 
$$x_i > x_j$$
,  $b_{i,j} > b_{i,i}$  or  $b_{j,j}$ 

: Different-size coagulation occurs faster than that between similar size coagulation...

Monodisperse particles becomes polydisperse...

Polydisperse particles becomes monodisperse..

\* Self-preserving,  $\sigma_{q,ultimate} \approx 1.4$ 

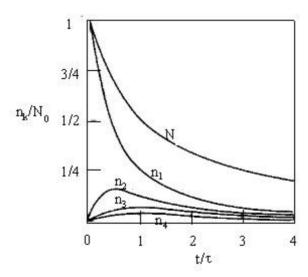
For monodisperse particles in air at 1atm and 20°C

$$b = \frac{8kT}{3\mu} = K = 3.0 \times 10^{-16} C_c$$
 ,  $\frac{m^3}{s}$ 

Then

$$\frac{dn_i}{dt} = \frac{K}{2} \sum_{i+j=k} n_i n_j - K n_i \sum_{j=1}^{\infty} n_j$$

Integration yields



Summing up over  $i = 1, \infty$ 

$$\sum_{i=1}^{\infty}\frac{dn_i}{dt} = \frac{K}{2}\sum_{i=1}^{\infty}\sum_{i+j=k}n_in_j - K\!\sum_{i=1}^{\infty}n_i\!\sum_{j=1}^{\infty}n_j$$

**Therefore** 

$$\frac{dN}{dt} = -\frac{K}{2}N^2$$

Integration yields

$$N(t) = \frac{N_0}{1 + N_0 Kt}$$

Since  $N\left(\frac{\pi}{6}x^3\right) = constant$  and  $N_0x_0^3 = Nx^3$ 

$$\frac{x(t)}{x_0} = \left(\frac{N_0}{N(t)}\right)^{1/3}$$

#### Example.

The initial number concentration of a magnesium-oxide fume is  $10^7/cm^3$ , and the particles are  $0.2\mu m$  in diameter. Determine the time required for the concentration to decrease to  $10^6/cm^3$ . Assume simple monodisperse coagulation at  $20^{\circ}C$  with a constant K of  $5\times10^{-16}m^3/s$  [ $5\times10^{-10}cm^3/s$ ]. What is the average particle diameter at the end of this period?

$$10^{6} \text{cm}^{-3} = \frac{10^{7} \text{cm}^{-3}}{1 + 10^{7} \text{cm}^{-3} \cdot 5 \cdot 10^{-10} \cdot \frac{\text{cm}^{3}}{\text{s}} t} \text{ solve } \rightarrow 1800 \cdot \text{s}$$

$$x = 0.2 \cdot 10^{-6} \text{m} \cdot \left( \frac{\frac{10^7}{\text{cm}^3}}{\frac{10^6}{\text{cm}^3}} \right)^{\frac{1}{3}} = 4.309 \times 10^{-7} \text{m} \qquad 0.439 \text{um}$$

# 9.4 General Dynamic Equation

Population balance for particles

$$\frac{dn(v)}{dt} = D \nabla^{2} n(v) - \overline{U} \cdot \nabla n - \nabla \cdot (n \overline{V})$$

Accumulation Diffusion convection migration

$$+\left(\frac{dn(v)}{dt}\right)_{nucl}+\left(\frac{dn(v)}{dt}\right)_{coag}+\left(\frac{dn(v)}{dt}\right)_{coad}$$

where

$$\begin{split} \left(\frac{\partial n(v)}{\partial t}\right)_{vcl} &= R_N \cdot \delta(v^*) \\ \left(\frac{\partial n(v)}{\partial t}\right)_{coag} &= \frac{1}{2} \int_0^v b(v',v-v') n(v') n(v-v') dv' - n(v) \int_0^\infty b(v,v') n(v') dv' \\ \end{split}$$

$$\left(\frac{\partial n(v)}{\partial t}\right)_{cond} = -\frac{\partial I}{\partial v}$$

where I: particle current

the number of particles per unit time per unit volume of gas

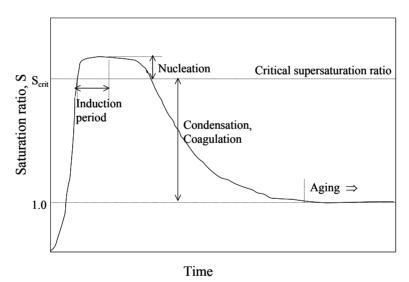
passing the point v

Since 
$$I(v) \approx n(v) \frac{dn}{dt}$$

$$\left(\frac{\partial n(v)}{\partial t}\right)_{cond} = -\frac{\partial \left(n(v)\frac{dv}{dt}\right)}{\partial v}$$

## 9.5 Some Comments on Particle Growth

## (1) Overall Growth



## (2) Effect of Growth Mechanisms on Particle Size Distribution

#### Nucleation

- Increase of particle number concentration
- Gives delta function in particle size distribution in given condition
- May cause accelerating the rate of coagulation

#### Condensation

- No effect on particle number concentration
- Results in monodisperse size distribution.

#### Coagulation

- Decreases in particle number concentration
- Gives polydisperse size distribution in growth process

## (3) Formation of Monodisperse Particles

- Maintain low rate of nucleation using low supersaturation
- Induce heterogeneous nucleation
  - \* Matijevic's method
- Allow the same growth time for all the particles by shortening the time of nucleation
- Suppress coagulation
  - · Using electrostatic repulsion (electrical double layer)
  - · Using adsorption of surfactants and macromolecules
  - · Rapid cooling followed by rapid dilution
- Use of Ostwald ripening (not for oxides)

# 9.5 Formation Methods of Nanoparticles

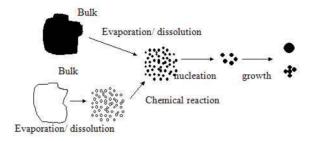
#### (1) Introduction

- \* Keys for NP preparation
  - Formation of high-degree supersaturation in narrow time or space
  - Suppression of aggregation
  - Monodisperse growth- diffusion-controlled growth/Ostwald ripening
- \* Classification of preparation methods
  - In terms of phase of medium for preparation

    Gas / liquid / aerosol / solid phases
  - In terms of method of "monomer" preparation

## Physical/chemical

## (2) Gas-phase preparation

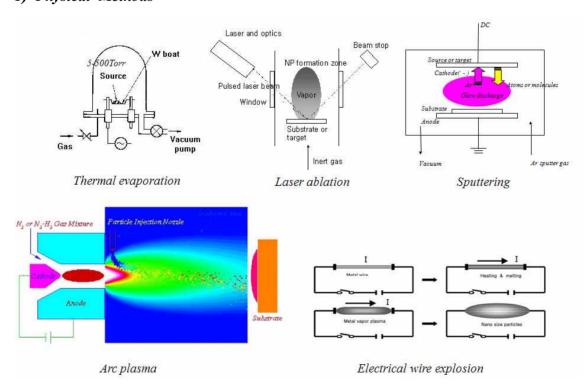


- Rapid increase in concentration of condensable vapor component by
  - · Vaporization/Sublimation: physical
  - · Chemical reaction

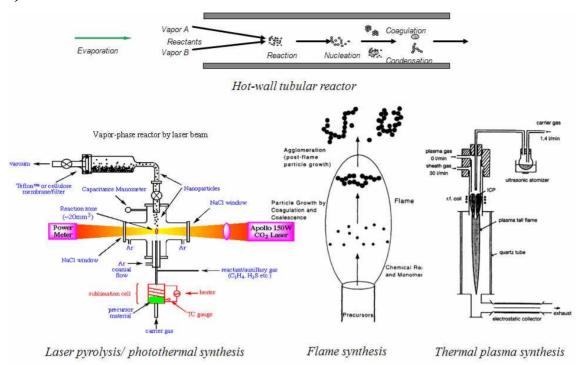
ex. 
$$Ti Cl_4(g) + O_2(g) = Ti O_2(s) + 2 Cl_2$$

- · Needs energy from hot wall, flame, laser, plasma...
- Followed by rapid cooling, expansion and dilution

## 1) Physical Methods



## 2) Chemical Methods



## (2) Liquid-Phase Preparation

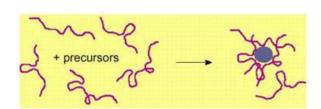
Mostly by chemical methods...

$$aA(l) + bB(l,q,s) \rightarrow cC(s) + dD(l)$$

- If C: highly insoluble, high chances to form very small and so many nuclei
- Results in giant aggregates composed of nanoparticles due to its high concentration and low mean free path in liquid phase.
- Requires to suppress aggregation of the nanoparticles
  - · Electrical double layer
  - · Surfactants
  - · Polymers
- Liquid-phase preparation:
  - · Delicate close to art...but robust...
  - · Involves many chemicals, many processes

# 1) Formation with polymeric stabilizer

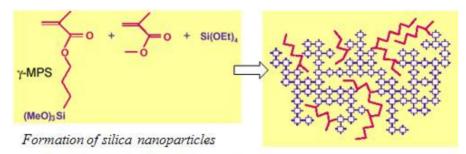
## - In polymer solution





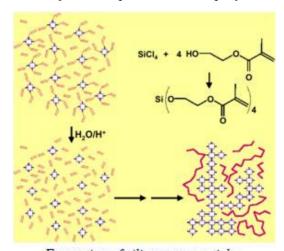
Iron oxide (left) without (right) with dextran

## - With simultaneous polymerization



 $\gamma$ -MPS=  $\gamma$ -methacryloyloxypropyl-trimethoxysilane

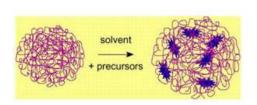
# - From a single precursor for nanoparticles and polymer

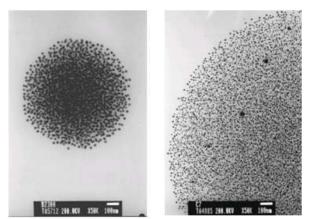


Formation of silica nanoparticles

# 2) Confined growth

- In polymer matrix

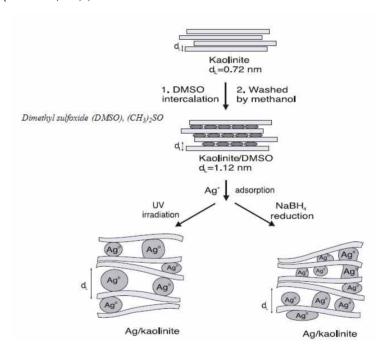




Silver NP in PVP matrix

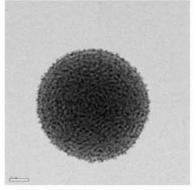
## - In layered materials

e.g. kaolinite(Al<sub>2</sub>Si<sub>2</sub>O<sub>5</sub>(OH)<sub>4</sub>)



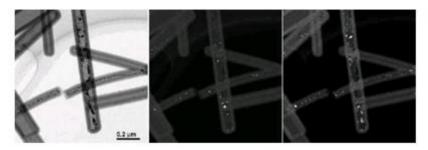
# - In porous materials

e.g. zeolites, mesoporous silica



Silver NP in mesoporous silica

#### - In nanotubes



BF, DF and conical DF image of Pt particles inside of SiO2-NTs

- Preparation of nanoparticles in microemulsion

## 3) Sol-Gel Methods

## Precursors

- Metal alkoxides,  $M(OR)_Z$ , in organic solvent
- Metal salts (chloride, oxychloride, nitrate..) in aqueous solution

### Basic mechanism

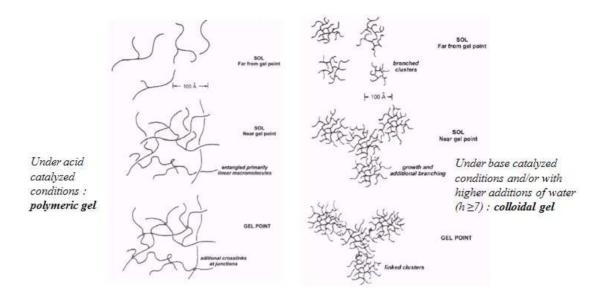
- Hydrolysis  $M-OR+H_2O = -M-OH + xROH$
- Polycondensation

$$-M-OH + RO-M = -M-O-M- + ROH$$
  
 $-M-OH + HO-M- = -M-O-M- + H_2O$ 

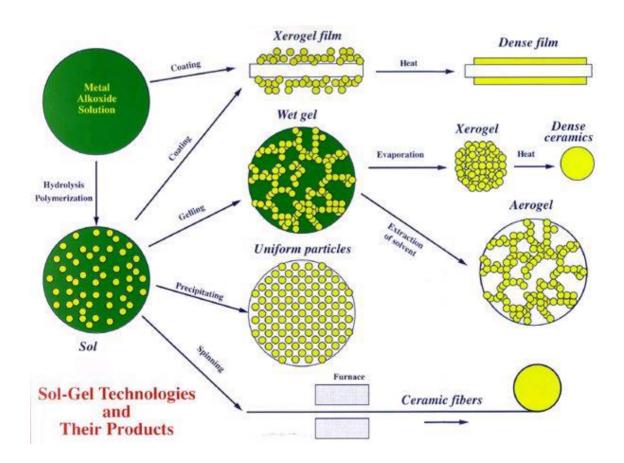
- · Occurs sequentially and in parallel
- · Usually  $M(OR)_n$ ,  $n>1 \rightarrow three-dimensional structures...$

### Gel formation

e.g. Sol-gel transformation for silica



<u>Supercritical extraction</u> → aerogels cf. xerogels



# Characteristics of aerogels

Porosity: 75-99%

Specific surface area:  $\sim >1,000 \text{m}^2/\text{g}$ 

cf. porosity of xerogel: 1-50%

- Very light, transparent
- Used in catalysts, sensor, electrodes, thermally and/or electrically insulating materials



