Experiment and CFD for heat management of CO<sub>2</sub> methanation in a bubbling fluidized-bed reactor

Ngo Ich Son, 임영일<sup>1,†</sup>, 이도연<sup>2</sup>, 서명원<sup>2</sup> 한경대학교; <sup>1</sup>HKNU; <sup>2</sup>KIER (limvi@hknu.ac.kr<sup>†</sup>)

In this study, the catalytic  $\mathrm{CO}_2$  methanation in PtG is experimentally and numerically investigated for a bubbling fluidized-bed (BFB) reactor. Due to the strong exothermic reactions, heat management is an important factor in improving reactor energy efficiency. The diluted reactant gas mixture  $(\mathrm{CO}_2/\mathrm{H}_2/\mathrm{N}_2=0.045/0.18/0.775$  in volume fraction) was fed at the bottom of BFB (ID = 0.05 m) filled by 0.15 m bed height of Ni-based commercial catalyst ( $\mathrm{d}_p=100~\mu\mathrm{m},\ r=2300~\mathrm{kg/m}^3$ ) to maintain the inlet superficial velocity at 400 °C of 0.03 m/s ( $\sim$ 3.5  $\mathrm{u}_{\mathrm{mf}}$ ). An Eulerian-Eulerian two-fluid computational fluid dynamics (EE-CFD) model incorporating with an empirical correlation of gas-solid interphase heat transfer and kinetic rate model was proposed for the BFB reactor. The EE-CFD results such as the bed expansion, temperature profile, the gas molar fraction of species,  $\mathrm{CO}_2$  conversion,  $\mathrm{CH}_4$  yield and producer gas purity along the reactor height were compared with experimental data. The effects of operating conditions on the heat management of the BFB reactor were analyzed from the EE-CFD simulation.